

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

VI. Onshore Treatment

1		
2		
3		
4		
5	VI. Onshore Treatment.....	1
6	A. Studies of Onshore Treatment.....	1
7	B. Advantages of Onshore Treatment Compared to Shipboard Treatment.....	3
8	1. Number of treatment plants and total treatment capacity	3
9	2. Constraints on treatment	4
10	3. Treatment methods available	5
11	4. Plant operation by trained water/wastewater treatment personnel	6
12	5. Reliability	6
13	6. Overall Effectiveness.....	7
14	7. Safety.....	7
15	8. Adaptability	8
16	9. Compliance monitoring and regulation	8
17	C. Issues Raised About the Feasibility of Onshore Treatment.....	9
18	1. Ballast discharge before arrival to reduce time spent at berth	9
19	2. Ballast discharge to reduce draft before arriving at berth	10
20	3. Delays	11
21	4. Cost recovery	11
22	5. Cost	12
23	D. Other Objections to Onshore Treatment.....	12
24	1. Invested effort.....	13
25	2. Timing	13
26	3. International issues.....	14
27	E. Cost of Onshore vs. Shipboard Treatment.....	16
28	1. Onshore treatment cost estimate for California.....	17
29	2. Onshore treatment cost estimate for the United States	19
30	3. Shipboard treatment cost estimates and comparison	20
31	F. Potential Effectiveness of Onshore Treatment in Removing, Killing or Inactivating Organisms.....	21
32	G. Conclusions and Recommendations	29
33		
34		
35	Appendix 1. Literature Review of Onshore Treatment Studies.....	32
36	Appendix 2. Cost Estimate Adjustments and Calculation of Annualized Costs.....	45
37	Appendix 3. Adjustment of the Cost Estimates in Brown and Caldwell (2007) to the Design Criteria in	
38	Brown and Caldwell (2008)	47
39	Appendix 4. Estimates of Treatment Plants and Capacities in Onshore and Shipboard Treatment	
40	Approaches for Milwaukee, Australia, California and the United States	50

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1	Appendix 5. Cost Analysis	59
2		
3	References Cited	68
4		
5		

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

Do not Cite or Quote This draft Subgroup product is a work in progress, does not reflect consensus advice or recommendations, has not been reviewed or approved by the chartered SAB, and does not represent SAB views or EPA policy.

Subgroup 4. Onshore Treatment, inclusion in response to Question 4

VI. Onshore Treatment

Onshore treatment involves either treatment facilities built on land or treatment facilities installed on a port-based treatment ship, which will be referred to as “on-land” and “treatment ship” approaches, respectively. Some reports have taken onshore treatment to mean the treatment of ballast water in existing wastewater treatment plants. This is considered here as a special case of on-land treatment which may or may not be feasible in specific circumstances. Currently, some oil-contaminated ballast water is discharged to on-land facilities designed to separate hydrocarbons from the water. Some studies have considered modifying these facilities to remove or kill organisms in ballast water, and this is also treated here as a special case of on-land treatment. Other reports have considered using existing water or wastewater treatment plants as sources of clean ballast water that could be loaded on ships and later discharged without further treatment, or onshore facilities that would pump hot water into a ship’s partially empty ballast tank to kill organisms in it (=external source treatment, Aquatic Sciences 1996). These approaches are not considered to be onshore treatment in this report. The discussion and assessment of onshore treatment in this report refers to treatment in onshore facilities that are built specifically and solely to receive and treat ships’ ballast water in order to remove or kill organisms, except where explicit reference is made to treatment in existing on-land treatment facilities.

The discussion includes a review of the literature on onshore treatment (§VI.A), a comparison of the strengths and possible weaknesses of onshore treatment relative to shipboard treatment (§§VI.B-VI.D), an analysis of costs relative to shipboard treatment (§VI.E), an assessment of the capability of onshore treatment to meet various levels of discharge standard (§VI.F), and a summary of conclusions and recommendations (§VI.G).

A. Studies of Onshore Treatment

Onshore treatment has been briefly commented on in several studies, but significantly analyzed in only a few (Table A1-1 in Appendix 1). Some studies concluded that onshore treatment is a technically feasible option either for the industry as a whole or for some part of the industry (NRC 1996; Oemke 1999; CAPA 2000; California SWRCB 2002; Brown and Caldwell 2007, 2008); none found it to be technically infeasible. A few concluded that cost or other factors could limit its use to part of the industry, but provided no data or analyses to support this (Victoria ENRC 1997; Dames & Moore 1998, 1999; Rigby & Taylor 2001a,b; California SLC 2009, 2010). Gauthier & Steel (1996) stated that onshore treatment is “considered a poor option,” citing Pollutech (1992) who drew no such conclusion but rather ranked onshore treatment higher than nearly all shipboard approaches. Dames & Moore (1999) stated that onshore treatment is

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

“considered to be less favorable than on-board treatment options” without saying who considered it so; Dames & Moore (1998) identified the source of this opinion as Oemke (1999),¹ who however made no such statement.² The U.S. EPA and U.S. Coast Guard reports that deal with ballast water management contain neither analyses nor significant discussions of onshore treatment (*e.g.* it is mentioned briefly in US EPA 2001, mentioned in a single sentence in Albert et al. 2010, and not mentioned at all in a discussion of ballast treatment technologies in US Coast Guard 2008). However, the potential for treating ballast discharges onshore has been repeatedly recognized in laws and regulations, and in international guidelines and treaty conventions (Appendix A1).

Four studies compared the effectiveness or costs of onshore and shipboard ballast water treatment. Pollutech (1992) ranked onshore treatment second in terms of effectiveness, feasibility, maintenance and operations, environmental acceptability, cost, safety and monitoring out of 24 ballast water management approaches for vessels entering the Great Lakes. AQIS (1993a) found onshore treatment to be cheaper than shipboard treatment in both single-port and nation-wide scenarios in Australia, concluding that onshore treatment facilities “are more economic and effective than numerous ship-board plants.” Aquatic Sciences (1996) estimated the costs of using treatment ships to treat ballast water discharge in the Great Lakes, and concluded that onshore treatment approaches are technically feasible, “more practical and enforceable” than shipboard treatment, and “offer the best assurance of prevention of unwanted introductions.” California SWRCB (2002) found onshore treatment to be the only approach to have acceptable performance in all three categories of effectiveness, safety, and environmental acceptability in a qualitative comparison with ten shipboard treatment alternatives. Cost estimates compiled by the U.S. Coast Guard (2002) also showed onshore treatment to be generally less expensive on a per metric ton basis than onshore treatment. Several other published comparisons of onshore and shipboard treatment consist of lists or brief discussions of their relative merits, none of which provide any significant analysis or data. Descriptions of these comparisons are provided in Appendix 1.

In addition to AQIS (1993a) and Aquatic Sciences (1996), two studies provided conceptual designs and cost estimates for onshore treatment for specific regions. CAPA (2000), an EPA-funded study, developed designs and cost estimates for the state of California, and Brown and Caldwell (2007, 2008) did the same for the Port of Milwaukee. Several studies have estimated the costs of modifying ships so they can discharge ballast water to onshore facilities; these costs vary considerably with ship type and size (Table A1-7 and Figure A1-2 in Appendix 1). The most recent and probably the most sophisticated of these studies were conducted by Glosten

¹ Cited “in review” in 1998.

² Oemke (1999) cited several advantages of onshore treatment (use of treatments not feasible on ships, easy adjustment of pH to optimal treatment conditions, easy removal of oxidant residuals), noted that it is a “very attractive” option for the VLCC portion of the fleet, but suggested that it will not be widely used otherwise because of ships’ practice of partially deballasting while approaching berths.

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

(2002) and Brown and Caldwell (2008), who explicitly based their estimates on designs that allow ships to deballast completely during the time needed for cargo loading at berth.

B. Advantages of Onshore Treatment Compared to Shipboard Treatment

Onshore ballast water treatment systems have several advantages relative to shipboard treatment, which have been cited in various studies.

1. Number of treatment plants and total treatment capacity

For shipboard treatment, a treatment plant must be installed on each ship. In nearly all cases these treat ballast water either during ballast uptake, during ballast discharge, or both (Table VI.B-1),³ and must be large enough to accommodate the ship's maximum ballast pumping rate (ABS 2010). This is assumed to be equal to a ship's total ballast pump capacity, which is often in the 1,000-2,000 MT/h range and can be as high as 20,000 MT/h (Table A4-1 in Appendix 4). The total treatment capacity needed is equal to the sum of the ballast pump capacities of all the ships. In contrast, in onshore treatment one plant serves a number of ships, and because all ships do not arrive and discharge ballast water simultaneously, the treatment capacity needed, even without any storage, will always be less than the sum of the maximum ballast discharge rates of the ships. However, some ballast water storage will always or nearly always be included in an onshore plant, and depending on the relative costs of storage and treatment can be sized to reduce the needed treatment capacity to the average ballast water discharge rate (e.g. see AQIS 1993a; Ogilvie 1995; CAPA 2000; Brown and Caldwell 2007, 2008).

Table VI.B-1. Percentage of shipboard ballast water treatment systems that treat during ballast uptake, ballast discharge, or both. Treatment phase and commercial availability (through 2009) from Lloyd's Register 2010, Tables 5 & 6. Type approval (though February 2010) from ABS 2010, Table 7.

³ Physical separation processes (filtration, electro-mechanical separation or hydrocyclones) all produce an untreated waste stream (backwash from filters or underflow from hydrocyclones), which essentially requires that these processes be conducted during ballast uptake so this untreated water can be discharged back to the source waters (Cohen & Foster 2000; California SLC 2010; Lloyd's Register 2010). UV is generally applied immediately after this initial particle-removal process, because it is less effective if particles are present in the water, and in some treatment systems is also applied, without further filtration/particle removal, during discharge (ABS 2010). Biocides are generally injected during uptake, to promote mixing and maximize contact time. Chlorine is generally injected (or created by electro-chlorination) immediately after particle removal both to enhance its effectiveness and to maximize contact time, and chlorine neutralization (which occurs nearly instantaneously) is then conducted during discharge. In all of these cases, which cover most of the treatment processes being used to address ballast water, the system must be sized to treat the maximum ballast flow rate on uptake or discharge. Deoxygenation appears to be the only treatment approach that is, in some systems, applied only during the voyage and not during either uptake or discharge (Lloyd's Register 2010; ABS 2010).

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Treatment Phase	All treatment systems (n=41)	Commercially available systems (n=21)	Type-approved systems (n=10)
Uptake only	37%	48%	50%
Discharge only	7%	4%	0%
Both	51%	48%	50%
Uptake or discharge	95%	100%	100%

Table VI.B-2 compares the estimated number of individual treatment plants and the total treatment capacity that would be needed for onshore vs. shipboard treatment in the Port of Milwaukee, Australia, California and the United States, over a 20-year (Milwaukee) or 30-year (other sites) project life. The onshore plants and capacities are based on adjusted estimates from the available studies (Brown and Caldwell 2008, AQIS 1993a and CAPA 2000, respectively), which are explained in Appendix 4.

Table VI.B-2. Treatment plant and capacity estimates for the Port of Milwaukee, Australia, California and the United States. Assumptions and methods are described in Appendix 4.

Site	Number of Treatment Plants		Total Capacity of Treatment Plants (MT/h)	
	Onshore	Shipboard	Onshore	Shipboard
Milwaukee	1	19	230	22,800
Australia	23	2,160	34,940	1,188,000
California	16	13,115	1,814	18,883,140
United States	314	83,200	35,549	119,475,200

Based on these estimates, the number of plants needed for shipboard treatment over the project period is between nearly 20 times and >800 times the number needed for onshore treatment, depending on the region. For the U.S. as a whole, shipboard treatment would require the installation of >260 times as many plants as onshore treatment. The treatment capacity needed for shipboard treatment is between >30 times and >10,000 times the capacity needed for onshore treatment, depending on the region; for the U.S. it is about 3,400 times what is needed for onshore treatment.

2. Constraints on treatment

Major constraints on shipboard treatment include limited space (Pollutech 1992; AQIS 1993a; Aquatic Sciences 1996; NRC 1996; Cohen 1998; California SLC 2010; Albert & Everett 2010), limited power availability (NRC 1996; Cohen 1998; California SLC 2010), limited treatment

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 time (NRC 1996; Oemke 1999) and an unstable platform (AQIS 1993a; Cohen 1998; Reeves
2 1999). These constraints are largely absent in onshore systems.

3
4 Installation plans for shipboard treatment plants usually place them within a ship's engine room,
5 where ballast pumps are located (NRC 1996). Aquatic Science (1996) noted that "modern ship
6 design tends toward the reduction of machinery space to maximize cargo capacity, with the
7 result that many modern engine rooms are cramped, allowing only sufficient space for necessary
8 maintenance." Similarly, the National Research Council (1996) noted that "ships are built to
9 carry maximum cargo, [so] non-earning space such as engine rooms...is reduced to a minimum.
10 In particular, engine rooms tend to have very limited space for additional equipment, although
11 the most convenient location for a treatment facility would be in or adjacent to the engine room
12 in which the ballast pumps are located." While it may be possible to expand treatment systems
13 into adjacent cargo spaces, this involves a costly "double-hit": in addition to the direct costs of
14 the equipment and its installation including piping and bulkhead penetrations to connect back
15 into the engine room, the reduction in cargo capacity reduces revenues.

16
17 AQIS (1993a) noted general concerns about restricted access and working space around
18 shipboard treatment equipment. Pollutech (1992) noted that many of the treatment options being
19 considered "could be more easily incorporated into [an onshore] facility in comparison to being
20 fitted into a vessel." The National Research Council (1996), Oemke (1999) and Rigby & Taylor
21 (2001b) noted that heat treatment may not work on short trips, and the same may be true for
22 biocide treatments that require significant contact time in ballast tanks, or time for neutralization.
23 The motion of a ship makes it difficult and costly to employ granular filtration methods,
24 requiring the use of pressurized containers (AQIS 1993a); Gauthier & Steel (1996) and the
25 National Research Council (1996) concluded that even with pressurized containers, space
26 limitations make this approach impractical. Engine vibrations and ship motions in rough seas
27 (Welschmeyer 2005; California SLC 2010), concerns about corrosion (Carlton et al. 1995; NRC
28 1996; Cohen 1998) and hazardous working conditions at sea (NRC 1996; Cohen 1998) may also
29 constrain the types of treatment processes or treatment equipment that can be used on ships, or
30 pose difficulties that require additional cost or effort to resolve.

31
32 *3. Treatment methods available*
33

34 Any treatment method used on ships can be used onshore; however, there are treatment methods
35 available for use onshore that cannot practically be used on ships because of space, stability, time
36 or safety constraints. These include such common and relatively inexpensive water or
37 wastewater treatment processes as settling tanks, flotation processes and granular filtration⁴
38 (AQIS 1993a; Gauthier & Steel 1996; NRC 1996; Victoria ENRC 1997; Cohen 1998; Reeves
39 1999; Cohen & Foster 2000; California SWRCB 2002) and the use of chlorine gas for

⁴ Sometimes called media filtration or deep media filtration.

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

disinfection (Cohen & Foster 2000), as well as microfiltration, ultrafiltration and reverse osmosis processes (AQIS 1993a; California SLC 2010). Settling tanks and flotation processes require a steady free surface and are feasible only in onshore applications (AQIS 1993a; Gauthier & Steel 1996; Cohen 1998; Reeves 1999). Granular filtration could in theory be employed shipboard in pressurized containers (AQIS 1993a), but space requirements make it impractical (Gauthier & Steel 1996; NRC 1996; Cohen 1998; Reeves 1999; Cohen & Foster 2000).

4. Plant operation by trained water/wastewater treatment personnel

It is expected that shipboard treatment plants will be operated and maintained by ships' regular crewmembers, in addition to their existing duties (NRC 1996; California SLC 2010). Several researchers have noted that the quality of operation and maintenance will probably suffer (Pollutech 1992; AQIS 1993a; Aquatic Sciences 1996; Reeves 1998), or that operation of treatment systems by better trained personnel in onshore plants would result in superior performance (Cohen 1998; California SWRCB 2002; Brown & Caldwell 2007; California SLC 2010). Maintenance and repair work are also more likely to be done effectively, and needed replacement parts obtained more quickly, in onshore plants (AQIS 1993a; Aquatic Sciences 1996; Cohen 1998; Cohen & Foster 2000).

AQIS (1993a) noted that in shipboard systems "treatment equipment would be subject to operation, repair and maintenance by the crew. With the standards of ship maintenance in some cases having slipped badly for the both hull and machinery, it may be assumed in these cases that ballast water treatment systems would not be accorded a high priority for maintenance and could be easily by-passed or operated at sub-optimal efficiency." Aquatic Sciences (1996) noted with regard to shipboard treatment that "crew standards with respect to operating and maintenance capability in the deep sea fleet are unpredictable at best....there are no guarantees of their effectiveness...Filtration, strainers, or other high maintenance systems are particularly vulnerable" and "are least likely to stay in service particularly in shipboard applications." California SWRCB (2002) concluded that "a landbased treatment facility operated by professional wastewater treatment specialists would allow a better control of the treatment processes." Brown and Caldwell (2007, 2008) concluded that one advantage of onshore treatment "operated and maintained by experienced treatment operators" is "better control in ensuring that the desired level of ballast water treatment occurs."

5. Reliability

Operation and maintenance by trained wastewater treatment staff, as well as easier, safer, more consistent and more predictable working conditions (including better access and working space; less corrosive conditions; stability; fewer, more predictable time constraints; and freedom from hazardous or emergency conditions that may pertain at sea), as discussed above and below, should produce more reliable and consistent performance. Reliability can be further improved by

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 building redundancy into an onshore plant, but this will often be impractical in a shipboard plant
2 due to space constraints. Relative costs will also make this far more difficult in shipboard
3 systems, due to the large difference in the core treatment capacity need in shipboard vs. onshore
4 applications (estimated above at about 3,400 times as much capacity needed in shipboard than in
5 onshore applications to treat U.S. ballast water discharge). Because of this, adding some extra
6 capacity (30% for example) to each treatment plant to provide redundancy in case part of the
7 system breaks down or is taken offline for maintenance would entail a much greater industry-
8 wide cost for shipboard than for onshore treatment approaches, even without considering the
9 added costs due to shipboard space constraints.

10
11 Some studies point out that bypassing a shipboard treatment plant designed to operate inline
12 during ballasting, or failing to employ it effectively, at any point in the history of the treatment
13 plant could compromise the quality of later discharges, since organisms, including cysts or other
14 resting stages, retained in large numbers in sediments at the bottom of ballast tanks could
15 contaminate properly-treated ballast that is loaded later (AQIS 1993a; Reeves 1998). In a section
16 titled “The Virgin Tank,” Reeves (1998) explains that “the concept is that water will always be
17 treated in-stream at the time of intake and the tank will be maintained in a consistently pristine
18 condition...The problem with this appealing concept is that one filter breakthrough or failure to
19 religiously maintain and use the system...throughout the voyages around the world to ports such
20 as Bombay and Naples by a foreign crew will contaminate the tank and vitiate the protection to
21 be achieved when the vessel later shows up in a U.S. or Canadian port.”

22
23 *6. Overall Effectiveness*

24
25 Many of the above advantages—the absence of the space, time and power constraints that
26 characterize shipboard applications, the ability to use common and effective water and
27 wastewater treatment processes that are impractical or impossible at sea, the operation and
28 maintenance of treatment systems by trained personnel, and the greater ability to install extra
29 capacity and redundancy—will tend to make onshore treatment more consistently effective at
30 removing or killing organisms in ballast water. Other factors—cost factors that make it possible
31 to concatenate a larger and more effective set of treatment processes in onshore plants (discussed
32 in later sections), and the greater adaptability of onshore treatment discussed below—also raise
33 the potential effectiveness of onshore relative to shipboard treatment. Dames & Moore (1999)
34 reported that onshore treatment provided “complete control of effectiveness,” and Lee et al.
35 (2010) stated that compliance with a zero discharge standard is feasible only with on-land
36 treatment.

37
38 *7. Safety*

39
40 Shipboard treatment involves restricted working spaces and difficult and potentially hazardous
41 working conditions at sea (AQIS 1993a; Cohen 1998; Cohen & Foster 2000), which increases

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the risk of accidents related to treatment processes or materials. For processes that involve the storage and use of biocides or other hazardous chemicals, there is greater risk of harm to personnel in shipboard than in onshore applications (AQIS 1993a; Carlton et al. 1995; Reeves 1998; Cohen 1998; Cohen & Foster 2000) and greater risk of accidental discharge to the environment (Pollutech 1992; AQIS 1993a; Carlton et al. 1995). In addition, because many of the cheapest and most effective physical separation processes cannot be used onboard ships (as discussed above), to achieve a given level of treatment shipboard treatment systems will likely rely on biocides to a greater extent than will onshore systems.

AQIS (1993a) concluded that “the control of occupational health and safety issues would...provide the most difficulty in shipboard systems, particularly if hazardous chemicals are involved,” and also noted concerns regarding “hazardous environments created by the treatment equipment, e.g. heat, UV, mechanical movements,” etc. on board ships. Lloyd’s Register (1995, cited in Reeves 1998) stated that “both inorganic and organic biocides would present a range of health and safety problems related to storage of chemicals, compatibility with cargo carried on board as well as direct and indirect handling of chemicals by crew members.” The National Research Council (1996) noted that while “safety issues associated with handling chemicals on board a ship may be of concern,” the volume of such chemicals may be small and it should be possible to train ships’ crews to handle them safely. Cohen (1998) noted “concerns about crew safety or wear or stress on the ship (*i.e.* concerns over storage and use of toxic chemicals, corrosion or thermal stresses that arise with various on-board treatments).” Regarding the risk of environmental damage, Pollutech (1992) observed that “the risk of a spill [in onshore plants] would be less than that for all vessels carrying the same chemicals.”

8. Adaptability

There are greater space restrictions on ships than onshore, and, as discussed in a later section, structural cost factors make treatment components a much smaller part of the total cost of treatment in onshore than in shipboard applications. As a result, if at some point after the initial installation or construction of a treatment plant it is determined that additional treatment components are needed, it is both physically and financially easier to retrofit them in onshore than in shipboard applications. Similarly, it is financially easier to upgrade or replace existing treatment components in onshore than in shipboard applications, even if these changes involve no additional space requirements. Brown and Caldwell (2008) noted that onshore systems would “provide treatment flexibility, allowing additional treatment processes to be added or modified as regulations and treatment targets change”

9. Compliance monitoring and regulation

The effort and cost of regulatory monitoring and enforcement needed to achieve a given level of compliance is expected to be much less for a relatively small number of onshore, domestic

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1 treatment plants compared to a much larger number of mobile, transient, sometimes foreign-
2 owned⁵ shipboard treatment plants (roughly 300 times as many plants needed to treat all
3 discharges into U.S. waters, according to the estimates above), which are accessible only when in
4 a U.S. port for (usually) a short period of time (AQIS 1993a; Ogilvie 1995; Aquatic Sciences
5 1996; Cohen 1998; Dames & Moore 1999; Oemke 1999; Cohen & Foster 2000; California
6 SWRCB 2002; Brown and Caldwell 2007). Several studies noted the difficulty of monitoring
7 shipboard treatment and the greater ease of monitoring and inspecting onshore treatment (AQIS
8 1993a; Cohen 1998; Dames & Moore 1999; Cohen & Foster 2000; California SWRCB 2002;
9 California SLC 2010).

10
11 AQIS (1993b) reported that one advantage of onshore treatment is that it is “the only
12 arrangement where:

- 13 • responsibility for monitoring, control and effectiveness is totally in the hand of authorities at
14 the destination port;
- 15 • beneficiaries of treatment (coastal water users, fisheries and aquaculture industries etc.) have
16 physical evidence of controls in place;
- 17 • there is no reliance on actions from originating port authorities or ship operators to ensure
18 that treatment is effective.”

19 Both Dames & Moore (1999) and California SWRCB (2002) noted the value of having the
20 receiving port authorities be responsible for the operation and maintenance of treatment systems.
21 Dames & Moore (1999) noted that onshore treatment removed “the need for reliance on ships’
22 logs (which can potentially be falsified).” Aquatic Sciences (1996) recommended that new
23 initiatives in ballast water treatment “focus on compliance, enforcement and monitoring issues as
24 a major driving force in the selection criteria.”
25

26 **C. Issues Raised About the Feasibility of Onshore Treatment**
27

28 Five issues have been identified in the literature.
29

30 *1. Ballast discharge before arrival to reduce time spent at berth*
31

32 Several studies noted that some vessels, including bulk carriers, may discharge part of their
33 ballast water before arriving at berth so they can complete discharge by the time the cargo is
34 loaded (AQIS 1993a; Oemke 1999; Cohen & Foster 2000; CAPA 2000; Rigby & Taylor 2001a).
35 AQIS (1993a) noted that for a bulk carrier “normal vessel operation may involve dumping up to
36 20% of ballast water in coastal waters as it approaches port.” However, AQIS (1993b) also noted
37 that if the “rate at which the cargo is to be loaded is such that the ship’s ballast pumps can
38 discharge ballast at a comparable or higher rate, deballasting may be carried out entirely while

⁵ Roughly 20% of the 40,000 cargo ships estimated to be subject to the EPA’s Vessel General Permit are foreign-flagged (Albert & Everett 2010). What fraction are foreign-owned is not known.

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1 alongside the berth.” One solution, then, is to outfit a ship’s ballast water system with pipes and
2 pumps that are large enough to allow the ship to unload ballast water as quickly as it loads cargo.
3 The issue is then reduced to the question of whether this is so expensive that the overall cost of
4 treating ballast water onshore becomes untenable. Glosten (2002) and Brown and Caldwell
5 (2007, 2008) developed cost estimates for retrofitting bulk carriers and other vessels to allow
6 them to deballast at berth during the time they load cargo, and these estimates are used in the
7 cost analysis in §VI.E.

8
9 *2. Ballast discharge to reduce draft before arriving at berth*

10
11 Several studies also noted that a ship might discharge ballast water before arriving at berth to
12 reduce draft in order to cross over a shallow bar or to enter a shallow channel (Cohen 1998;
13 Dames & Moore 1998, 1999; Oemke 1999; CAPA 2000, Rigby & Taylor 2001a; California
14 SWRCB; California SLC 2010). None of these studies, however, provide any data indicating
15 whether this is a rare or a more common circumstance. Several studies note the possibility of
16 addressing this issue (at least in some circumstances) by offloading some ballast water to a barge
17 before arriving at berth, a practice that some ships at some ports routinely do for liquid cargo (a
18 process called lightering) (AQIS 1993a; Carlton et al. 1995; Dames & Moore 1999; CAPA 2000;
19 Rigby & Taylor 2001a; Glosten 2002; California SWRCB 2002). This would have some cost, of
20 course. Dames & Moore (1998) suggested that a treatment ship (that is, not just a barge that can
21 receive ballast water and transport it to shore, but a vessel with an installed treatment plant
22 designed to receive *and treat* ballast water from cargo ships) could “service deep-drafted high-
23 risk arrivals that need to deballast during approach to shallow berths at neap tide periods,”
24 though whether this would be generally feasible or cost-effective is unclear.

25
26 An approach applicable to all situations, and probably the least cost option in most, is for the
27 shipping industry to adjust operationally, that is, to send cargo to a port on ships that can reach
28 berth without having to partially deballast first. The industry already makes this type of
29 operational adjustment all the time—that is, shipping companies take into consideration the
30 characteristics of the port and the channels that must be traversed when deciding which ship to
31 send to which port carrying which cargo, and they have a great deal of expertise in selecting the
32 most efficient, least cost option to do so. Adding the additional constraint of not being able to
33 discharge ballast water before arriving at port would have some cost, but the industry is well set
34 up to make operational decisions to minimize this cost. Theoretically, the overall cost could be
35 significant or insignificant, depending on how commonly this circumstance occurs and on how
36 much it would take to work around it, and there doesn’t appear to be any quantitative data
37 available on either of these questions. However, one knowledgeable authority stated that ships
38 today are sent to harbors that can accommodate them without have to reduce their draft, and that
39 ships that shed ballast coming into a harbor nearly always do so in order to reduce deballasting
40 time at berth (Captain Philip Jenkins pers. comm. to Fred Dobbs).

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 *3. Delays*

2
3 Several studies have noted the possibility of costly delays (Dames & Moore 1998, 1999; Cohen
4 1998; Oemke 1999; Cohen & Foster 2000; CAPA 2000). In all cases, these appear to be a
5 restatement of issues 1 and 2. That is, (1) if a ship is not allowed to start deballasting before
6 arriving at berth *and* its ballast discharge system isn't modified so it can discharge at berth in the
7 time it takes to load cargo, then it could be delayed; and (2) if a ship is sent to a port where it
8 must cross shallows that require it to reduce its draft and it is not allowed to discharge ballast
9 water into the water, then it must either offload part of its ballast or cargo to another vessel,
10 which will involve some delay, or in some cases it might be possible to wait until the tide rises,
11 which will also involve some delay. Since delaying a ship is generally quite costly, the least cost
12 option will in most cases be to outfit the ship with ballast pipes and pumps that are large enough
13 to allow deballasting to occur as rapidly as cargo loading, and to ship cargo to ports on ships that
14 can enter those ports without having to offload ballast or cargo or wait for higher tides.

15
16 *4. Cost recovery*

17
18 Some studies stated that cost recovery could be an issue (Dames & Moore 1998; Oemke 1999).
19 While there is a cost recovery question associated with onshore treatment—that is, regional
20 governments and ports will have to decide whether they want to pay for part or all of the cost of
21 ballast water treatment, or whether ships will be charged a fee for having their ballast treated in
22 an onshore plant with the fees set at a level that pays for the construction and operation of the
23 plant—there doesn't appear to be any cost recovery issue that is a barrier to implementation of
24 onshore treatment.⁶ In reality, regional governments and ports face the same decision with
25 shipboard treatment, though it's not as obvious. Thus, a regional government (such as a state or a
26 country) could adopt ballast water discharge requirements and then reimburse ships for the costs
27 incurred in meeting those requirements, if it decided it was in the public interest to do so.
28 Alternately, ports could offer to reimburse ships that voyage to the port for any ballast treatment
29 costs incurred on that voyage, in order to entice shipping companies to use the port. Or regional
30 governments and ports could decide to let the ships pay for the cost of treating their ballast water.

⁶ Of the studies that mention cost recovery, the only actual discussion of the issue (beyond a few word mention of it) appears to be in Cohen & Foster (2000), as follows: "One question that arises with on-shore treatment is who would pay for the construction and operation of treatment facilities, the ships or the ports? If ships were required to treat their ballast water discharges and onshore treatment was the cheapest approach, either shipping companies, ports or, conceivably, independent entrepreneurs might choose to construct treatment facilities. If ports or independent parties were to do so, they could recover costs and turn a profit by charging ships appropriate fees for receiving and treating their ballast water. A potential advantage to the shipping industry of on-shore treatment is that plant construction costs are more likely to be subsidized by federal or state governments—just as the cost of constructing wastewater treatment plants was subsidized during the implementation of the Clean Water Act—than would the cost of constructing or installing treatment plants on board ships. For example, low-interest or no interest loans are available for the construction of on-shore facilities to treat ballast water in California, through the State Revolving Fund administered by the State Water Resources Control Board, which is a form of subsidy."

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1
2 *5. Cost*
3

4 Several studies mention one or another element of the cost of onshore treatment, or mention
5 costs generally, as a disadvantage of onshore treatment (Cohen 1998; Dames & Moore 1998:
6 “expensive connection problems”; Dames & Moore 1999: “high costs of construction”; Rigby &
7 Taylor 2001b: “high cost of the installation”; California SLC 2010: costs “may be
8 prohibitive...the acquisition of land for facility construction...would be...costly”). There clearly
9 are substantial costs associated with treating ballast water onshore, just as there are with treating
10 ballast water onboard ships. Whether it is an advantage or a disadvantage of onshore compared
11 to shipboard treatment depends on whether the total costs of onshore treatment are higher or
12 lower than the total costs of shipboard treatment that achieves the same task (that is, that meets
13 the same regulatory standard). This is discussed in §VI.E below on costs.
14

15 Dames & Moore (1999) states that onshore treatment is “an expensive option for ports with a
16 low incidence of high-risk arrivals.” In making this statement Dames & Moore assumed that
17 only ballast discharges identified as high risk would be required to undergo treatment, rather than
18 all ballast discharges, but the general point is valid: constructing and operating a treatment plant
19 in ports that receive little ballast water will result in high costs per MT of ballast water treated at
20 that plant. Both the AQIS (1993a) study in Australia and the CAPA (2000) study in California
21 made the same point, and proposed alternatives. AQIS (1993a) proposed deploying barges to
22 receive ballast discharges in smaller ports, which would periodically transport the collected
23 ballast water to treatment plants located in the larger ports. CAPA (2000) decided that building a
24 treatment plant in Port Hueneme, which according to the data available to them received only
25 687 MT/y (an average of <500 gallons/day), would not make any sense. Instead they proposed
26 an on-land pipe system and storage tank to receive and store ballast water, which would
27 periodically (every 6-7 months in their plan) be barged to treatment plants in the ports of Los
28 Angeles or Long Beach, a short distance to the south. The statement that onshore treatment
29 requires building a separate treatment plant everywhere that a ship comes into port, as it is
30 sometimes framed, is not correct. At small ports the question of whether to build an onshore
31 treatment plant, or to build an onshore storage tank with periodic transport of stored ballast to
32 larger ports, or to deploy a barge to collect and transport ballast water from ships, will be decided
33 based on the relative costs of each.
34

35 **D. Other Objections to Onshore Treatment**
36

37 During Committee discussions, three issues were raised regarding onshore treatment that don’t
38 question either its feasibility or its effectiveness. Rather, these are policy arguments that other
39 considerations make shipboard treatment a more desirable option than onshore treatment, and
40 that therefore the U.S. should not set discharge standards based on the effectiveness of onshore

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 treatment that are too demanding for shipboard treatment systems to meet. These three
2 arguments have to do with the effort already spent on developing shipboard treatment; the
3 relative amount of time it would take to implement shipboard or onshore approaches; and
4 considerations related to potential disparities between U.S. ballast water regulations and
5 regulations in some other countries.

6
7 *1. Invested effort*

8
9 One argument is that various parties have in one way or another spent a lot of time working on
10 shipboard treatment systems, and the U.S. should not waste this effort by adopting such
11 demanding discharge standards that shipboard treatment would be abandoned in favor of more
12 effective onshore approaches.

13
14 In economic and business analysis this is described as a decision based on retrospective or sunk
15 costs (often called the “sunk cost fallacy” or “sunk cost effect” in economics and behavioral
16 studies, and the “Concorde fallacy” in game theory, referring to the failure of the British and
17 French governments to pull out of the economically disastrous Concorde jet project). While
18 various hypotheses have been advanced to explain why individuals or institutions sometimes
19 make decisions based on sunk costs, these decisions are considered to be irrational or
20 maladaptive (e.g. Arkes & Blumer 1985; Keasey & Moon 2000). Rather, future effort or
21 investment should be made where the benefits or returns are expected to be greatest, not where
22 effort or investment has been made in the past.

23
24 *2. Timing*

25
26 Another argument is that it will take longer to build onshore plants than to install shipboard
27 plants, and that the U.S. should therefore adopt less demanding discharge standards that can be
28 met by shipboard plants. First, it’s not clear that building onshore plants will take any longer than
29 installing shipboard plants. Barring site-specific difficulties that could occur with some
30 individual plants, the expected length of time needed to complete the design, permitting and
31 construction of an onshore treatment plant is about 30 months for plants larger than 10 mgd
32 (≈ 1580 MT/h) (Robert Bastian, US EPA Office of Water, pers. comm. in email to Dr. Charles
33 Haas, 12/06/10). Virtually all the onshore plants needed in the U.S. would be smaller than 10
34 mgd⁷ and should take less time to complete. Shipboard treatment systems can presumably be

⁷ CAPA (2000) estimated that onshore ballast water treatment in California would require two 1 mgd plants and eight 0.1-0.2 mgd plants. When these estimates are adjusted upward with more recent and complete ballast water discharge data, the largest plant needed is still only 3.7 mgd, and 80% are less than 0.6 mgd. Nationwide ballast water discharge data (Miller et al. 2007) are compiled by regions known as Captain of the Port Zones (COTPZs), which may cover more than one port. These data, after being increased to adjust for reporting rates, show only five COTPZs in the U.S. with average ballast water discharge rates at or above 10 mgd: Houston-Galveston (22 mgd),

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 installed on new vessels during construction without significantly increasing construction time.
2 However, for an existing vessel, either installing a shipboard plant or modifying its ballast
3 system so it can discharge ballast water to an onshore facility would require the vessel to be out
4 of service either in drydock or at wharfside where this work could be done. This occurs
5 infrequently, with hull inspections with or without drydocking typically occurring every 2.5-5
6 years, though the out-of-service time for these activities may not always be long enough to allow
7 treatment system installation or ballast system modification (Captain Phil Jenkins, pers. comm.
8 to Dr. Fred Dobbs)⁸. Thus the critical path for construction of either shipboard or onshore
9 treatment in the U.S. is the installation of a shipboard treatment system or the modification of the
10 ballast pipe system on the 40,000 existing cargo ships (plus 29,000 other vessels) that are
11 expected to be subject to the VGP, and not the onshore or new vessel construction work. The
12 time to complete the construction of either shipboard or onshore treatment is thus likely to be
13 about the same.

14
15 An additional factor to consider is the time needed to develop an effective monitoring and
16 enforcement program. As discussed earlier, a larger and more costly program would be needed to
17 monitor and enforce shipboard treatment (involving tens of thousands of transient, globally-
18 roaming treatment plants) than onshore treatment (involving hundreds of stationary plants on
19 U.S. soil). Depending on how aggressively the EPA moved to develop a monitoring and
20 enforcement program, this could affect the overall time to implementation, favoring onshore
21 treatment over shipboard treatment.

22
23 Finally, even if shipboard treatment *could* be implemented quicker than onshore treatment, it is
24 not clear that earlier implementation would outweigh the various benefits of onshore treatment.
25 To reach that determination would require considering information both about the relative timing
26 of implementation for the two approaches and about their relative effectiveness and other
27 characteristics (including safety, reliability, adaptability, amenability to monitoring and
28 regulation, cost, etc.).

29
30 *3. International issues*

31
32 A final argument was made that even if onshore treatment is the most effective approach to
33 protecting U.S. waters, the U.S. should not base its discharge standards on it because adopting
34 weaker standards that can be met with shipboard treatment would allow ships to install shipboard
35 systems, and this might indirectly benefit certain other countries that are unlikely to build the
36 facilities that would be needed to treat ballast water onshore. This was described as a matter of

Prince William Sound (20 mgd), Duluth (16 mgd), New Orleans (14 mgd) and Saulte St. Marie (10 mgd). It appears that at most a handful of onshore ballast water treatment plants will be needed that are larger than 10 mgd.

⁸ The implementation schedule in the IMO convention (which phases in the D2 discharge standards over an 8 year period) was designed at least in part to address the necessity of installing shipboard plants during infrequent out-of-service periods.

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

"environmental justice." This is a complex issue, which we discuss in three parts.

Would U.S. adoption of weaker discharge standards based on the capabilities of shipboard treatment systems benefit certain other countries? For this to occur, the benefitting country would have to be unable or unwilling to implement either ship-based or onshore treatment if the U.S. adopted strong standards that required onshore treatment⁹, and be both willing and able to adopt discharge requirements and a compliance monitoring and enforcement regime that is sufficient to persuade ships to operate installed treatment systems on voyages to the benefitting country, if the U.S. adopted weaker standards that could be met with shipboard treatment. It's unclear whether any countries fall into this category.

Would U.S. adoption of weaker discharge standards benefit the global environment? U.S. adoption and implementation of stronger standards and more effective onshore treatment would better protect U.S. waters from invasions, and in so doing would benefit other countries as well by preventing U.S. waters from serving as "stepping stones" from which these invasions may reach other countries. In addition, if the U.S. adopted stronger standards and onshore treatment, this could encourage other countries to do so as well, which would have further global benefits. So even if some countries did benefit in an indirect way from the U.S. adopting weaker standards, those countries and other countries could lose out in other ways, and the net effect on the global environment could be detrimental.

Is this an environmental justice issue? The legal basis for the federal environmental justice program is Executive Order 12898, which charged federal agencies with "identifying and addressing, as appropriate, disproportionately high and adverse human health or environmental effects of its programs, policies, and activities on minority populations and low-income populations in the United States and its territories and possessions, the District of Columbia, the Commonwealth of Puerto Rico, and the Commonwealth of the Mariana Islands." The home page of the EPA's Environmental Justice section defines environmental justice as "the fair treatment and meaningful involvement of all people regardless of race, color, national origin, or income with respect to the development, implementation, and enforcement of environmental laws, regulations, and policies. EPA has this goal for all communities and persons across this Nation."

The argument that certain other countries would benefit if the U.S. adopted weaker standards based on shipboard treatment, even if true, does not constitute an environmental justice issue as defined by the federal government or the U.S. EPA. First, it doesn't involve disparities in health or environmental effects, in treatment by the EPA, or in opportunities for involvement in EPA

⁹ We note that onshore treatment plants have the potential to become profit centers for receiving ports or countries—that is, onshore plants could charge ships fees that would pay for the costs of construction and operation *and* turn a profit (Cohen & Foster 2000)—thus perhaps making them somewhat more likely to be constructed in other countries if the U.S. leads the way.

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 actions.¹⁰ Second, it doesn't involve disparities or distinctions based on race, color, national
2 origin, or income. Third it doesn't involve disparities between individuals or communities within
3 the United States. What it involves is differences in environmental regulations between
4 countries, and an argument that certain types of differences in these regulations would be more
5 advantageous to certain countries than other types of differences. Environmental laws and
6 regulations in the U.S. often differ from those in other countries and these differences do not
7 constitute an environmental injustice as defined by U.S. law, no matter what the indirect effects
8 of those differences may be.¹¹
9

10 **E. Cost of Onshore vs. Shipboard Treatment**
11

12 As the review of past studies on onshore treatment showed, there is broad agreement that
13 onshore treatment of ship's ballast water is technically feasible: (1) we have the technological
14 ability to transfer ballast water off of cargo ships and into an on-land receiving system, a
15 treatment ship, or a transport barge; (2) we can move ballast water through pipes on land to
16 storage tanks or treatment plants; (3) there is a broad array of proven technologies that we can
17 use to treat ballast water in a treatment plant on land or on a treatment ship; and (4) in an on-land
18 treatment plant (and to a substantial degree on a treatment ship), we can concatenate probably as
19 many of these treatment technologies as we need to achieve the desired (potentially very
20 rigorous) level of treatment (see the §VI.F on the effectiveness of onshore treatment). The
21 question of feasibility, then, really comes down to cost. Can this be done at a total cost that is not
22 obviously impractical? It is beyond the scope of this committee's work to try to figure out what
23 the maximum acceptable total cost of treating the nation's ballast discharges might be. A far
24 simpler question is: How does the total cost of treating ballast water onshore compare to the total
25 cost of treating ballast water on ships? If shipboard treatment is considered economically
26 feasible¹², and onshore treatment is not significantly more costly, then onshore treatment must be
27 economically feasible also.
28

29 In the following discussion we compare the total estimated costs of the onshore or shipboard

¹⁰ The circumstances described in this argument do not correspond to any of the environmental justice issues described in EPA guidance documents (US EPA 2004, 2010b).

¹¹ One final point worth noting is that the usual remedy for disparities in environmental protection that are believed to be unjust is to strengthen environmental protection where it is weak, not to weaken it where it is strong.

¹² We don't know whether any government body has determined that shipboard treatment of ballast water is economically feasible, and we are not making that determination here. We only note that shipboard ballast water treatment systems have been installed and are operating on some ships (Lloyd's Register 2010); that the interest and activities of the shipping industry, equipment manufacturers and investors in shipboard treatment systems suggest that they believe that it is economically feasible; and that the IMO's ballast water convention, the ratification of that convention by various port states, the laws and regulations adopted by various U.S. states, the regulations proposed by the U.S. Coast Guard, and the convening of this committee and the charge questions provided to it by the Office of Water suggest that those entities also believe that shipboard treatment is economically feasible.

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 treatment needed to deal with the ballast water discharged into California waters, and then
2 extend those estimates to all U.S. waters. The California estimate is based on the most relevant
3 and complete estimate of onshore treatment costs available, the CAPA (2000) study. This is
4 augmented by other available sources of information to estimate onshore treatment costs that
5 were not included in the CAPA estimate. Shipboard treatment costs for California are based on
6 the estimated number of distinct ships arriving in California ports and the ballast pump capacities
7 of those ships, derived from data in Ballast Water Reporting Forms submitted by ships arriving
8 in California since January 1, 2000 (California SLC 2010), and on recently published estimates
9 of shipboard treatment system costs in Lloyd's Register (2010).

10
11 For the U.S., onshore costs are estimated by multiplying the California onshore cost by the ratio
12 between the total amount of ballast water, from both foreign and domestic sources, discharged
13 into U.S. waters and the amount of such discharge into California waters. These figures are
14 derived from data in Ballast Water Reporting Forms submitted by ships arriving in U.S. ports in
15 2004-2005, which is the most recently compiled data available (Miller et al. 2007). Shipboard
16 treatment costs are based on the number of distinct ships estimated to be subject to the VGP
17 (Albert & Everett 2010) and the recent estimates of shipboard treatment costs (Lloyd's Register
18 2010). As no data are available on the ballast pump capacities of the ships subject to the VGP
19 (Ryan Albert, pers. comm. in SAB public conference call 10/26/10), we applied the ballast pump
20 capacity figures for ships arriving in California (California SLC 2010).

21
22 Costs were adjusted to current (June 1, 2010) U.S. dollars and annualized costs were calculated
23 as described in Appendix 2. Because of differences in the estimated working lifetimes of
24 different project elements (Appendix 2), annualized costs were used for the comparisons.
25 Sensitivity analyses were conducted by varying the inputs over a range of estimates to test the
26 robustness of the results (**Appendix 5-to be completed**).

27
28 *1. Onshore treatment cost estimate for California*
29

30 The basic onshore cost estimate is a modified version of the EPA-funded CAPA (2000) estimate
31 for treating ballast water discharged in California waters. As described in Appendix 1, this
32 estimate includes the following elements: piping from berths to plants; storage tanks; a treatment
33 system consisting of coagulation, flocculation, filtration and UV disinfection, plus solids
34 thickening, dewatering and disposal; and discharge through an outfall pipeline. The treatment
35 system costs include both capital costs and O&M (operations and maintenance) costs. For the
36 other elements only capital costs were estimated, as the O&M costs were assumed to be minor.
37 To produce the California onshore cost estimate, we modified the CAPA (2000) estimate as
38 follows:

- 39 • CAPA (2000) used an inappropriate method that underestimated annualized costs. We
40 estimated annualized costs as described in Appendix 2.
- 41 • CAPA (2000)'s estimated costs were adjusted to June 1, 2010 dollars as described in

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Appendix 2 (the adjusted estimates by port are shown in Table A1-4 in Appendix 1).

- As explained in Appendix 4, the CAPA (2000) estimate was based on some of the earliest available ballast discharge data, which covered less than a year, only included data from ships that had traveled overseas, and suffered from low reporting rates. CAPA (2000) annualized the data but did not correct for the other data limitations. We estimated total ballast water discharge in California based on the most recent data as described in Appendix 4, and adjusted the CAPA (2000) estimated costs upward to correspond to our estimate of total ballast discharge.
- Land costs were not included in the CAPA (2000) estimate. We estimated these from the sale prices for vacant land near California's ports advertised on the Internet, with the size of the properties needed based on estimated treatment plant footprints and the storage tank footprints from CAPA (2000), adjusted to larger storage and treatment capacity requirements based on our larger estimate for total ballast water discharge.
- The costs of retrofitting existing ships and constructing new ships with ballast water pipes and pumps designed to allow ships to discharge ballast water to onshore facilities were not included in the CAPA (2000) estimate. We estimated these costs based on the literature on ship retrofit costs reviewed in §VI.A and Appendix 1¹³, and the number of distinct ships arriving at California ports and subject to ballast water regulations, derived in Appendix 4 from California State Lands Commission data.

These successive adjustments are shown in Table VLE-1. The details of these calculations are provided in Appendix 5 (to be completed).

¹³ We used the cost estimates in Glosten (2002) and Brown and Caldwell (2008), which were based on engineering designs with large enough pipes and pumps to enable ships to complete deballasting at berth during the time it takes to load cargo, thereby eliminating the economic basis for the practice of partially deballasting en route to berth.

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Table VI.E-1. Modified cost estimates for onshore treatment in California. See text for explanation.

Ship Retrofit/ Modification	Capital Costs Pipes	Storage Tanks	Treatment Plants	Outfalls	Treatment- Annual O&M	Total Annualized Costs
Cost estimates from CAPA (2000):						
—	117,110,400	60,755,000	17,941,300	1,100,000	1,608,308	8,171,865
...with costs annualized per Appendix 2:						
—	117,110,400	60,755,000	17,941,300	1,100,000	1,608,308	14,417,370
...adjusted to June 1, 2010 dollars per Appendix 2:						
—	146,950,130	76,235,374	22,512,743	1,380,280	2,018,105	18,090,918
...adjusted to our updated estimate of total ballast water discharge:						
—	475,813,801	282,764,077	40,689,651	5,119,587	7,485,338	59,811,874
...with land cost and ship retrofit/modification costs included:						
1,763,426,722	475,813,801	377,358,051	57,239,651	5,119,587	7,485,338	181,755,388

2. Onshore treatment cost estimate for the United States

The cost of the onshore components of onshore treatment (onshore pipes, storage, treatment and outfalls) for ballast water discharged into U.S. waters was estimated by multiplying the cost estimate for the onshore components in California (annualized and adjusted to June 1, 2010 dollars and to our estimate of total California ballast water discharge, with land costs included) by the ratio between the annual ballast discharge in the two regions. The cost for ship retrofit/modification was estimated as for California by applying the estimate of per ship costs, derived from the literature, by the estimated number of distinct ships subject to ballast water regulations. The resulting estimates are shown in Table VI.E-2. Details are in Appendix 5 (to be completed).

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Table V.I.E-2. Cost estimates for onshore treatment in the United States. See text for explanation.

Ship Retrofit/ Modification	Capital Costs			Treatment- Annual O&M	Total Annualized Costs
	Pipes	Storage Tanks	Treatment Plants		
10,755,934,145	9,320,836,392	7,392,161,911	1,121,281,931	100,288,871	146,632,177
					2,012,990,586

3. Shipboard treatment cost estimates and comparison

Shipboard treatment cost estimates for both California and the United States were based on the numbers of ships expected to be subject to ballast water regulations, as estimated in Appendix 4, and the average costs of installing treatment systems on those ships. For both regions the average maximum ballast pumping rate for ships was assumed to be 1,436 MT/h, which is the California average estimated in Appendix 4. The estimated average cost of an installed shipboard treatment system was based on the eight treatment systems for which type approval is reported as received or pending in Lloyd's Register (2010) or ABS (2010), and for which capital cost data were provided for both 200 and 2,000 MT/h treatment plants (Table 5 in Lloyd's Register 2010). The capital cost for a 1,436 MT/h plant was interpolated for each of these eight systems, and the average of these was used as the estimated average cost. The results, as total annualized costs, are \$462,468,478 for shipboard treatment in California (roughly 2.5 times the annualized onshore costs) and \$2,939,174,661 for the United States (about 50% greater than the onshore costs). The sensitivity tests in Appendix 5 show that the general results—that the total costs of onshore treatment are of the same order as or somewhat less than the total costs of shipboard treatment, for treatment comparable to that of currently available shipboard systems—are robust.

One other important point can be derived from these data. In onshore treatment, the treatment cost (capital plus O&M) is a modest fraction of the total cost: about 6% of the total in California, and about 11% of the total in the United States. Ship retrofitting, onshore pipe systems and storage tanks are each a larger fraction of the total cost. In shipboard treatment, however, all of the cost is treatment cost. This means that if an additional amount is spent to improve the effectiveness of the treatment process, for example by concatenating additional treatment processes and perhaps doubling or trebling the cost of the treatment component, the cost of shipboard treatment would increase proportionally (or more than proportionally if the additional processes or equipment impinge on the cargo space), but the cost of onshore treatment would increase only fractionally. This is illustrated by Table V.I.E-3, which shows that at higher levels of treatment the cost advantage of onshore treatment is substantially greater. This cost partitioning is also the source of some of onshore treatment's greater adaptability: treatment processes and equipment can be substantially modified, updated, augmented or even largely

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

replaced as experience dictates, without greatly increasing the total cost of treatment.

Table VLE-3. Changes in the ratio of total shipboard to onshore costs as the spending on treatment increases.

Increase in spending on treatment processes and equipment	Ratio of total shipboard costs to total onshore costs in:	
	California	United States
1x (no increase)	2.54	1.46
2x	4.79	2.63
3x	6.80	3.60
5x	10.20	5.08
10x	16.36	7.37

F. Potential Effectiveness of Onshore Treatment in Removing, Killing or Inactivating Organisms

Table VI.F-1 and Figure VI.F-1 show the allowable concentrations in different organism categories for several ballast water discharge standards, which span the range of proposed requirements.¹⁴ Table VI.F-2 provides statistics on organism concentrations measured in unexchanged, untreated ballast water at the ends of voyages (IMO 2003). These statistics were developed by researchers working with the International Maritime Organization. The data are not from a random sampling of vessels or voyages, but rather from vessels sampled in the relatively few port areas where researchers have been funded to do this type of work; nevertheless, this is the best compilation of data available. The statistics were provided for four organism groups: zooplankton, phytoplankton, bacteria and virus-like particles (VLPs). Generally, the zooplankton fraction (collected with nets with mesh sizes of 55-80 µm) is considered to correspond approximately to organisms in the >50 µm size class, and the phytoplankton fraction (collected with sieves with mesh sizes of <10 µm or counted in unconcentrated samples) is considered to correspond approximately to organisms in the 10-50 µm size class.

¹⁴ The standards also include public health protective limits for three indicator bacteria species or groups (toxicogenic *V. cholerae*, *E. coli* and intestinal enterococci), but since there are no data available on the mean concentration of these indicator bacteria in untreated, unexchanged ballast water on which to base an analysis, they are not treated further in this section.

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Table VI.F-1. Ballast water discharge standards for four organism classes.

	>50 μm per m^3	10-50 μm per ml	Bacteria per ml	Viruses per ml
US Negotiating Position	0.01	0.01	–	–
IMO D2	10	10	–	–
USCG Phase 1	10	10	–	–
USCG Phase 2	0.01	0.01	10	100
California Interim	no detectable	0.01	10	100
California Final	no detectable	no detectable	no detectable	no detectable

Figure VI.F-1. Ballast water discharge standards.

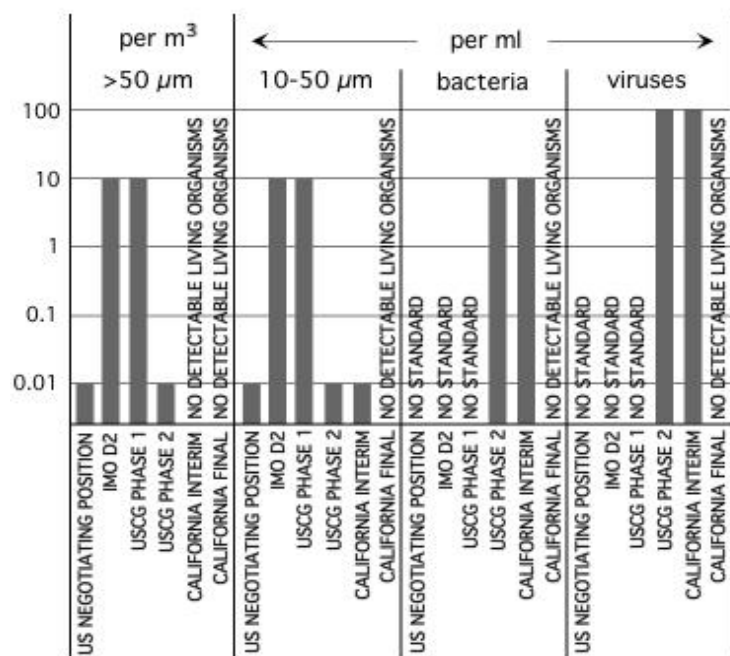


Table VI.F-2. Organism concentrations in untreated, unexchanged ballast water. Data from IMO (2003).

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

n (# of tanks sampled) =	Zooplankton 429 per m³	Phytoplankton 273 per ml	Bacteria 11 per ml	VLPs 7 per ml
maximum	172,000	49,716	1,900,000	14,900,000
mean	4,640	299	830,000	7,400,000
median	400	13.3	–	–
mode	100	0.001	–	–
minimum	0	0.001	240,000	600,000

Table VI.F-3 shows the log reductions from the maximum, mean, median and modal concentrations represented by several of the discharge standards, assuming that the zooplankton and phytoplankton sampled correspond to organisms in the >50 µm and 10-50 µm size classes, respectively. Relative to the mean concentrations in untreated, unexchanged ballast water, the IMO D2 and USCG Phase 1 standards require a 2.7 log reduction in the concentration of organisms in the >50 µm class and a 1.5 log reduction in the 10-50 µm class; with no overall reduction for bacteria or viruses. The USCG Phase 2 standard requires a 5.7 log reduction in the >50 µm class and 4.5-4.9 log reductions in the 10-50 µm class, bacteria and viruses. The required reductions relative to median values are smaller, by ≈1-1.5 log.

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Table VI.F-3. Log reductions required by different discharge standards.

	>50 µm per m³	10-50 µm per ml	Bacteria per ml	Viruses per ml
USCG Negotiating Position				
reduction from maximum	7.2	6.7	no reduction	no reduction
reduction from mean	5.7	4.5	no reduction	no reduction
reduction from median	4.6	3.1	no reduction	no reduction
reduction from mode	4.0	no reduction	no reduction	no reduction
IMO D2; and USCG Phase 1				
reduction from maximum	4.2	3.7	no reduction	no reduction
reduction from mean	2.7	1.5	no reduction	no reduction
reduction from median	1.6	0.1	no reduction	no reduction
reduction from mode	1.0	no reduction	no reduction	no reduction
USCG Phase 2; and California Interim (except for >50 µm)				
reduction from maximum	7.2	6.7	5.3	5.2
reduction from mean	5.7	4.5	4.9	4.9
reduction from median	4.6	3.1	no data	no data
reduction from mode	4.0	no reduction	no data	no data

With regard to what can be achieved by onshore treatment, the US EPA requires that drinking water treatment systems for surface water sources be capable of at least 3-5 log reductions in *Giardia*¹⁵ and 4-6 log reductions in viruses, depending on the quality of the source water (US EPA 1991). Several common drinking water filtration technologies are generally capable of 3-4 log reductions in protists and bacteria and 2-4 log reductions in viruses (Tables VI.F-4 to VI.F-6).

¹⁵ A protozoan with a flattened, pear-shaped active form (trophozoite) measuring around 3 x 9 x 15 µm and an ellipsoid cyst averaging 10-14 µm long.

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 **Table VLF-4. Examples of achievable log reductions for protists.**

Treatment	Parameter	Log reduction	Reference
<u>EXISTING STANDARDS</u>			
US EPA requirement for drinking water treatment, depending on the quality of the source water	<i>Giardia</i>	3-5	US EPA 1991
<u>FILTRATION AND/OR SEDIMENTATION PROCESSES</u>			
Coagulation-flocculation-sedimentation-filtration	<i>Cryptosporidium</i>	2	LeChevallier & Au 2004
Coagulation-flocculation-sedimentation-filtration	<i>Giardia</i>	3-3.6	US EPA 1991, 1997b; LeChevallier & Au 2004
Coagulation-flocculation-sedimentation-filtration	protozoa	≥4	LeChevallier & Au 2004
Coagulation-flocculation-dual media filtration	<i>Cryptosporidium</i>	≥2.3	LeChevallier & Au 2004
Coagulation-flocculation-dual media filtration	<i>Giardia</i>	≥3.3	LeChevallier & Au 2004
Dissolved air flotation	protozoa	3	WHO 2008
Granular filtration	<i>Cryptosporidium</i>	≥2.7	LeChevallier & Au 2004
Granular filtration	<i>Giardia</i>	≥4.4	LeChevallier & Au 2004
Granular high-rate filtration	protozoa	3	WHO 2008
Slow sand filtration	<i>Giardia</i>	4	US EPA 1997b
Slow sand filtration	<i>Cryptosporidium</i>	3	LeChevallier & Au 2004
Slow sand filtration	<i>Cryptosporidium</i>	>4	NESC 2000a
Bank infiltration	protozoa	4	WHO 2008
Bank infiltration	algae & diatoms	4.8-7.2	LeChevallier & Au 2004
High-rate clarification	algae	3.9	LeChevallier & Au 2004
High-rate clarification	diatoms	4.5	LeChevallier & Au 2004
High-rate clarification	protozoa	4	WHO 2008
Pre-coat filtration	protozoa	4	WHO 2008
Microfiltration (0.2 µm)	<i>Cryptosporidium</i>	5.3	LeChevallier & Au 2004
Microfiltration (0.2 µm)	algae	6.4	LeChevallier & Au 2004
Microfiltration (0.2 µm)	<i>Giardia</i>	>6	LeChevallier & Au 2004
Microfiltration (0.2 µm)	<i>Cryptosporidium</i>	>6	LeChevallier & Au 2004
Microfiltration or ultrafiltration	<i>Giardia</i>	>5-6	NESC 1999
Microfiltration or ultrafiltration	<i>Cryptosporidium</i>	>4.4 to >6.9	LeChevallier & Au 2004
Microfiltration or ultrafiltration	<i>Giardia</i>	>4.7 to >7.0	LeChevallier & Au 2004
Microfiltration or ultrafiltration	protozoa	complete removal	LeChevallier & Au 2004
Nanofiltration or reverse osmosis	<i>Giardia</i>	complete removal	NESC 1999
Microfiltration, ultrafiltration, nanofiltration or reverse osmosis	<i>Giardia</i>	complete removal	US EPA 1997b
Ultrafiltration, nanofiltration or reverse osmosis	protozoa	complete removal	WHO 2008
<u>BIOCIDES</u>			
Ozone with 5 min. contact	<i>Giardia</i>	3	US EPA 1997b
<u>UV DISINFECTION</u>			
UV at 5 mWs/cm ²	<i>Giardia</i>	2	WHO 2008
UV at 10 mWs/cm ²	<i>Cryptosporidium</i>	3	LeChevallier & Au 2004

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Table VI.F-5. Examples of achievable log reductions for bacteria.

Treatment	Parameter	Log reduction	Reference
<u>FILTRATION AND/OR SEDIMENTATION PROCESSES</u>			
Coagulation-filtration	total & fecal coliform	3	Wang et al. 2006
Coagulation-flocculation-sedimentation-filtration	<i>Clostridium perfringens</i>	3.1	LeChevallier & Au 2004
Slow sand filtration	total coliform	4	LeChevallier & Au 2004
Pre-coat filtration	bacteria	3	WHO 2008
4-m bankside infiltration	bacteria	≥4	WHO 2008
Microfiltration (0.2 µm)	heterotrophic bacteria	3.3	LeChevallier & Au 2004
Microfiltration (0.2 µm)	total coliform	4.3	LeChevallier & Au 2004
Microfiltration	bacteria	4	WHO 2008
Microfiltration	<i>Bacillus subtilis</i>	5.6-5.9	LeChevallier & Au 2004
Microfiltration plus nanofiltration	<i>Bacillus subtilis</i>	8-11	LeChevallier & Au 2004
Ultrafiltration	total & fecal coliform	≥6-7	Wang et al. 2006
Ultrafiltration (0.01 µm)	total coliform	≥7	LeChevallier & Au 2004
Nanofiltration or reverse osmosis	bacteria	complete removal	US EPA 1997b
Ultrafiltration, nanofiltration or reverse osmosis	bacteria	complete removal	WHO 2008
<u>BIOCIDES</u>			
3 mg/l chlorine (20 min. contact)	total & fecal coliform	3-4	Wang et al. 2006
4.5 mg/l chlorine (20 min. contact)	total & fecal coliform	≥5-6	Wang et al. 2006
0.1-0.2 mg/l ozone (1 min. contact)	<i>Mycobacterium avium</i>	3	LeChevallier & Au 2004
0.11 mg/l ozone (15 min. contact)	total & fecal coliform	4	Wang et al. 2006
1 mg/l ozone (15 min. contact)	total & fecal coliform	5-6	Wang et al. 2006
<u>UV DISINFECTION</u>			
UV at 0.65 mWs/cm ²	<i>Vibrio cholerae</i>	4	LeChevallier & Au 2004
UV at 20 mWs/cm ²	<i>Streptococcus sp.</i> , <i>Vibrio anguillarum</i> , <i>Pasturella piscicida</i>	3	Sugita et al. 1992
UV at 20 mWs/cm ²	<i>Escherichia coli</i>	4	LeChevallier & Au 2004
UV at 30 mWs/cm ²	<i>Salmonella typhi</i>	4	LeChevallier & Au 2004
UV at 31 mWs/cm ²	<i>Bacillus subtilis</i> spores	4	LeChevallier & Au 2004
UV at 60-90 mWs/cm ²	<i>Bacillus subtilis</i>	4	US EPA 1997b

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Table VI.F-6. Examples of achievable log reductions for viruses.

Treatment	Parameter	Log reduction	Reference
<u>EXISTING STANDARDS</u>			
US EPA requirement for drinking water treatment, depending on the quality of the source water	viruses	4-6	US EPA 1991
<u>FILTRATION AND/OR SEDIMENTATION PROCESSES</u>			
Flocculation-sedimentation	viruses	2.5	Guy et al. 1997
Coagulation-filtration	Coxsackie B3 virus	2	Wang et al. 2006
Coagulation-flocculation-sedimentation-filtration	viruses	3	US EPA 1991
Coagulation-flocculation-sedimentation-filtration	somatic coliphage	3.5	LeChevallier & Au 2004
Granular high-rate filtration	viruses	3	WHO 2008
4-m bank infiltration	viruses	4	LeChevallier & Au 2004; WHO 2008
Slow sand filtration	viruses	4	WHO 2008
Flocculation-sedimentation-rapid sand filtration-activated charcoal column-chlorination	viruses	>5.3	Guy et al. 1997
Microfiltration (0.2 µm)	total culturable virus	2.7	LeChevallier & Au 2004
Microfiltration (0.2 µm)	male-specific coliphage	3.7	LeChevallier & Au 2004
Ultrafiltration (0.01 µm)	MS-2 bacteriophage	≥6	LeChevallier & Au 2004
Ultrafiltration (0.01 µm)	MS-2 bacteriophage	≥6.5	LeChevallier & Au 2004
Nanofiltration or reverse osmosis	viruses	complete removal	US EPA 1997b; NESC 1999
Ultrafiltration at lower pore sizes, nanofiltration or reverse osmosis	viruses	complete removal	WHO 2008
<u>BIOCIDES</u>			
1 mg/l ozone (15 min. contact)	Coxsackie B3 virus	4	Wang et al. 2006
Ozone (5 min. contact)	enteric viruses	4	US EPA 1997b
Ozone (≈5 sec. contact)	MS-2, Hepatitis A	>3.9 to >6	US EPA 1997b
Lime softening at pH>11	viruses	4	WHO 2008
<u>UV DISINFECTION</u>			
UV at 6-16 mWs/cm ²	Hepatitis A	4	LeChevallier & Au 2004
UV at 23-30 mWs/cm ²	Poliovirus	4	LeChevallier & Au 2004
UV at 30 mWs/cm ²	Coxsackie AZ virus	4	LeChevallier & Au 2004
UV at ≈30 mWs/cm ²	Rotavirus	3	US EPA 1997b
UV at ≈40 mWs/cm ²	Rotavirus	4	US EPA 1997b
UV at 40-50 mWs/cm ²	Rotavirus	4	LeChevallier & Au 2004
UV at 60-90 mWs/cm ²	MS-2 bacteriophage	4	US EPA 1997b
UV at 50-100 mWs/cm ²	MS-2 bacteriophage	4	LeChevallier & Au 2004
UV at 90-140 mWs/cm ²	viruses	4	NESC 2000b
UV at 186 mWs/cm ²	Adenovirus	4	LeChevallier & Au 2004

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Membrane filtration technologies are capable of greater reductions (>4-6 log). In many of the membrane filtration assessments the remaining organism concentrations were below detection limits, and some documents describe these filters as “absolute barriers” that achieve “complete removal” of protozoans (by microfiltration—US EPA 1997b; LeChevallier & Au 2004; or by ultrafiltration—WHO 2008), of bacteria (by ultrafiltration—WHO 2008; or by nanofiltration—US EPA 1997b), and of viruses (by nanofiltration—US EPA 1997b; NESC 1999; WHO 2008). While in actual practice these membrane systems might not serve as true “absolute” barriers (e.g. due to pinpoint failures, especially over the course of operations), if they are operated and maintained as designed they are probably capable of producing effluent in which no organisms would be detected by any feasible ballast water compliance monitoring program.

UV disinfection can achieve 2-3 log reductions in protozoans and 3-4 log reductions in bacteria and viruses (Tables VI.F-4 to VI.F-6). Disinfection with biocides can achieve at least 3-log reductions in *Giardia*, 3-6 log reductions in bacteria, and 3-4 log reductions in viruses with appropriate doses and contact times (a few examples are given in Tables VI.F-4 to VI.F-6; higher doses or contact times might achieve even greater reductions). In the *Guidance Manual* for surface water treatment, the US EPA (1991) treats filtration and disinfection as additive processes: that is, a filtration process that can produce a 3 log reduction, and a disinfection process that can produce a 2 log reduction, in sequential combination are presumed to produce a 5 log reduction.

Thus, even without a disinfection step, several common drinking water filtration technologies that could be used onshore are capable of achieving the 1.5-2.7 log reductions from mean ballast water concentrations needed to meet the IMO D2 and USCG Phase 1 standards (Tables VI.F-4 to VI.F-6). Several combinations of filtration plus a single disinfection process appear capable of achieving the 4.5-4.9 log reductions needed to meet the USCG Phase 2 and California Interim requirements for viruses, bacteria and organisms in the 10-50 µm size class, and probably also the 5.7 log reduction needed to meet the USCG Phase 2 standard for organisms >50 µm. Treating with one or more additional disinfection process could produce yet greater log reductions.¹⁶ In comparison, in tests of type-approved shipboard treatment systems organisms in the >50 µm size class were reduced by at least 2.4-4.9 log, and organisms in the 10-50 µm size class by at least 1-3.8 log, depending on the treatment and the test conditions; bacterial counts were increased more often than they were reduced, and the tests provided no data on the effect on viruses (Table VI.F-7).

Some membrane filtration technologies that could be used in onshore plants have produced results of no detectable organisms in different organism classes. For example, judging from the microfiltration results cited in US EPA 1997b and LeChevallier & Au 2004, the microfiltration

¹⁶ Studies have shown that sequential combinations of some disinfectants produce reductions even greater than the sum of the disinfectants’ reductions when examined separately (LeChevallier & Au 2004).

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

unit that Brown and Caldwell (2008) included in the conceptual design for onshore treatment at the Port of Milwaukee would likely result in no detectable organisms in the effluent in both the >50 µm and 10-50 µm size classes. On the other hand, ultrafiltration or nanofiltration might be needed to leave no detectable bacteria or viruses in the filter effluent.

Table VI.F-7. Log changes demonstrated in tests of type-approved shipboard ballast water treatment systems.

Treatment	Test Conditions	Plankton >50 µm	Plankton 10-50 µm	Total Bacteria	Culturable Hetero- trophic Bacteria	Reference
Hyde Guardian	Shipboard	≥-2.4	-1.4	–	0.9	IMO 2009
Hyde Guardian	Land-based - 32 psu	≥-4.2	≥-1.1	-0.4	–	Veldhuis 2009; IMO 2009
Hyde Guardian	Land-based - 23 psu	≥-3.6	≥-1.2	0.1	–	Veldhuis 2009; IMO 2009
NEI	Land-based - 72 hr	-3.7	>-1	–	–	NEI 2007
NEI	Land-based - 96 hr	-4.0	>-1	–	–	NEI 2007
NEI	Land-based - 120 hr	>-4.5	>-1	–	–	NEI 2007
NEI	Land-based - 168 hr	>-4.0	>-2	–	–	NEI 2007
NEI	Land-based - freshwater 96 hr	>-4.8	>-2	–	–	NEI 2007
NEI	Land-based - <i>Artemia</i> 24 hr	-1.9	–	–	–	NEI 2007
NEI	Land-based - <i>Artemia</i> 48 hr	>-4.9	–	–	–	NEI 2007
NEI	Shipboard	≥-4.0	>-1	–	–	NEI 2007
SEDNA Peraclean	Land-based - high salinity	-4.7	>-3.5	0.5	≥2.8	Veldhuis & Fuhr 2008
SEDNA Peraclean	Land-based - low salinity	-4.9	>-3.8	0.3	1.4	Veldhuis & Fuhr 2008
SEDNA Peraclean	Shipboard	-3.4	>-3.6	0.0	<-2.7	Gollasch & Veldhuis 2008

G. Conclusions and Recommendations

• Available data suggest that onshore treatment of ballast water is technically feasible and at least as economically feasible as shipboard treatment.

By drawing on a set of technologies that are long-established and widely used in water or wastewater treatment, appropriately designed onshore treatment would appear to be substantially

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

more effective than shipboard treatment—by up to several orders of magnitude—probably at lower cost. The EPA should therefore use onshore treatment as the basis for assessing the ability of available technologies to remove, kill or inactivate living organisms that might otherwise be discharged from ballast tanks.

• Onshore treatment would require far less total capacity and far fewer treatment systems than would reliance on shipboard systems.

Because nearly all shipboard treatment systems being developed (including all type-approved systems) involve some in-line treatment process during ballasting or deballasting, the treatment capacity of a shipboard system must be at least as great as the maximum ballast pumping rate of the vessel it is installed in. These pumping rates can be as high as 20,000 MT/h on the largest vessels—requiring, within the engine room of such a vessel, the installation of a treatment plant whose capacity is greater than that of a wastewater treatment plant large enough to serve the population of the fifth largest city in the United States. With shipboard treatment, the cumulative installed capacity must equal the sum of the maximum pumping rates of all the vessels that install treatment plants. In contrast, with onshore treatment, capacity must equal the sum of the *average* rate of discharge of ballast water at each port, estimated at 0.03% of the capacity required for shipboard treatment if applied on a national scale. Onshore treatment also would require only around 0.4% of the number of treatment plants needed for shipboard treatment if applied on a national scale.

• Serious constraints that result from trying to fit a treatment plant within the engine room of a ship (including limited space, treatment time and available power, along with a lack of stability) are largely or entirely absent in onshore systems.

Common, effective and relatively inexpensive water and wastewater treatment processes that can be applied in onshore treatment cannot be used in shipboard situations. In addition, onshore plants, unlike shipboard plants, can be operated and maintained by trained water/wastewater treatment personnel. The combination of these circumstances means that onshore treatment plants are likely to be safer, more effective, more reliable and more adaptable than treatment plants that are installed and operated on board ships.

• The total cost of onshore treatment is estimated to be less than the total cost of shipboard treatment of equal effectiveness, especially if a high level of effectiveness is required. Lower total cost would result from the combination of smaller total treatment capacity and fewer treatment plants required, fewer physical constraints, greater availability of cheap and effective treatment processes, and lower costs to modify a ship's ballast water system to discharge to an onshore facility than to install a treatment plant on that ship.

• The effort and cost of monitoring and enforcement needed to achieve a given level of

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 **compliance is certain to be much less for a relatively small number of treatment plants**
2 **located in the U.S. compared to approximately 300 times as many mobile, transient and**
3 **sometimes foreign-owned shipboard plants which are available for inspection by U.S.**
4 **regulatory agencies only when in U.S. ports for short periods of time.**
5

6 **• The arguments against on-shore treatment are not supported by the majority of existing**
7 **information.**
8

9 Over the years some concerns have been raised about onshore treatment on the basis of
10 operational feasibility or cost, but none of these appear to be determinative. For example, it has
11 been argued that some ships must discharge some ballast water to reduce draft before arrival at
12 berth, but this is apparently a rare circumstance, which in any event can be addressed by the
13 normal operational procedure of sending ships to harbors that can accommodate them without
14 reductions in draft. Some ships also choose to discharge some ballast water before arrival at
15 berth in order to eliminate delays due to deballasting, but this issue can be resolved by installing
16 ballast pipes and pumps on ships that are large enough to allow full deballasting during the time
17 needed to load cargo (the costs of which are included in the cost comparison). The vague
18 concerns that have been raised about cost recovery also appear to lack substance: ships can be
19 charged for the service of ballast treatment. Ports or governments might or might not decide to
20 subsidize these costs, but in either case there doesn't appear to be any barrier to cost recovery.
21

22 More recently, three additional concerns have been raised about onshore treatment that are more
23 in the nature of policy arguments. First, even if onshore treatment is a superior approach that
24 could meet demanding discharge requirements, the U.S. should adopt less demanding
25 requirements that can be met by shipboard treatment because of the time and effort already spent
26 on developing and testing shipboard treatment. However, as discussed in Section VI.D., this
27 "sunk cost" argument is defective on economic grounds alone, aside from its environmental
28 implications.
29

30 Second, the U.S. should adopt the less demanding discharge requirements that can be met by
31 shipboard treatment because shipboard treatment could be implemented sooner than onshore
32 treatment. However, consideration of project critical paths suggests that construction of either
33 treatment approach would take about the same time.
34

35 Finally, that U.S. adoption of weaker shipboard-treatment-based discharge requirements would
36 indirectly benefit certain other countries, and not doing so would therefore be an act of
37 environmental injustice. However, the indirect benefits hypothesized to accrue to certain other
38 countries from U.S. adoption of these weaker standards are uncertain; the loss of the beneficial
39 effects of stronger U.S. discharge standards could result in net negative impacts globally; and the
40 circumstances do not constitute an environmental injustice as defined by the federal government.

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Appendix 1. Literature Review of Onshore Treatment Studies

Table A1-1 summarizes the various brief commentaries on and the relatively few analyses of onshore treatment that we found in ballast water reports and publications.

Table A1-1. Reports that discuss onshore treatment.

Report	Discussion	Conclusions
Pollutech 1992	Compares and ranks various shipboard and onshore treatment approaches.	Onshore ranks 2 nd out of 24 options, ahead of all but one shipboard system.
AQIS 1993a	Compares shipboard, on-land and treatment ship approaches.	On-land and treatment ship are cheaper and more effective than shipboard.
AQIS 1993b	Briefly discusses treatment ship and on-land treatment.	Onshore treatment is unlikely except in special circumstances.
Aquatic Sciences 1996	Compares shipboard, treatment ship, on-land and external source treatment.	Onshore is technically feasible and the most effective and cheapest approach.
NRC 1996	Briefly discusses advantages and disadvantages of onshore treatment.	Onshore remains an option.
Gauthier & Steel 1996	Mentions shipboard, treatment ship and on-land approaches.	Onshore is considered a poor option.
Victoria ENRC 1997	Briefly discusses onshore treatment.	Onshore is probably too costly at a large scale; may be viable at a smaller scale.
Greenman et al. 1997	Student report commissioned by the U.S. Coast Guard, largely reprising AQIS 1993a.	
Cohen 1998	Briefly discusses advantages and disadvantages of onshore treatment.	Onshore has many advantages and few disadvantages compared to shipboard.
Reeves 1998, 1999	Briefly discusses onshore treatment.	Lists onshore as an alternative.
Oemke 1999	Briefly discusses advantages and disadvantages of onshore treatment.	Onshore is feasible for some parts of the industry, such as VLCCs.
Dames & Moore 1998, 1999	Briefly discusses onshore treatment.	Onshore may be good option at oil export terminals with oil stripping plants.
Cohen & Foster 2000	Briefly discusses advantages and disadvantages of onshore treatment.	
CAPA 2000	EPA-funded study estimates the cost of onshore treatment for California.	Onshore is technically feasible.
Rigby & Taylor 2001a,b	Briefly discusses onshore treatment.	Cost, availability, quality control may prevent onshore development, but it might work for tankers that discharge oily ballast to

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

		onshore facilities.
US EPA 2001	Briefly mentions onshore treatment.	
California SWRCB 2002	Briefly discusses onshore treatment.	Onshore is an attractive option, at least for some parts of the industry.
Glosten 2002	Estimates upper-bound retrofit costs to discharge ballast to onshore facilities.	
NSF 2003	Mentions shipboard, onshore and operational options for the longer term.	Shipboard seems the most challenging approach.
Brown and Caldwell 2007, 2008	Develops designs and estimates costs for onshore treatment at Milwaukee.	Onshore is feasible; treatment ship is cheaper than on-land.
California SLC 2009, 2010	Briefly discusses advantages and disadvantages of onshore treatment.	Onshore might be suitable for terminals with regular vessel calls such as cruise ships, or for the Port of Milwaukee.

Four studies compared the effectiveness or costs of onshore and shipboard ballast water treatment. In a study for the Canadian Coast Guard, Pollutech (1992) scored and ranked a variety of ballast water management approaches for vessels entering the Great Lakes, including ballast water exchange and several shipboard and onshore treatments, in terms of effectiveness, feasibility, maintenance and operations, environmental acceptability, cost, safety and monitoring. On-shore treatment with discharge to a sanitary sewer (the only onshore treatment scenario analyzed) ranked second out of 24 treatment and management approaches analyzed in the report.

AQIS (1993a) developed conceptual designs and cost estimates to compare shipboard, on-land and treatment ship approaches to treating the ballast water discharged from 140,000-ton bulk carriers carrying 45,000 MT of ballast water with a maximum ballast pumping rate of 4,000 MT/h, and an annual discharge of 500,000 MT. The shipboard system that was analyzed consisted of a 50-µm in-line strainer employed during ballasting, plus the installation of high-level ballast tank offtake pipes to reduce the discharge of ballast sediments and settled cysts or spore stages. The cost of pump upgrades that might be needed to address head loss from the strainers was not included. The on-land facility was designed to handle the discharge from three bulk carriers per week and included 52,000 MT storage capacity with coagulation, flocculation, granular filtration and UV disinfection at a maximum treatment rate of 830 MT/h, and thickening, dewatering and land-fill disposal of residual solids. The cost of land acquisition and the cost of pipes needed to carry ballast water from the berths to the treatment plant were not included. The treatment ship alternative was based on converting a used 12,500 DWT bulk carrier and installing 4,000 MT of storage capacity and a treatment system similar to the on-land system but with a maximum treatment rate of 4,000 MT/h and using pressurized granular filters. The cost estimates, including the cost of retrofitting cargo ships with pipe modifications and

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

possible pump upgrades needed to allow discharge to an onshore treatment plant¹⁷, are summarized in Table A1-2. Based on the annualized cost per 1,000 MT of ballast water, treatment in an on-land facility (\$227-\$348/1,000 MT) is thus less than half to about two-thirds of the cost of treating it in a shipboard plant (\$529/1,000 MT). Treatment in a treatment ship is somewhat more or somewhat less expensive than treatment in a shipboard plant, depending on the utilization rate of the treatment ship (Table A1-2).

Table A1-2. Treatment cost estimates for shipboard, on-land and treatment ship approaches - single port scenario (AQIS 1993a). The figures have been adjusted to June 1, 2010 US dollars and annualized as described in Appendix 2. The number of ships is calculated as the number of bulk carriers (each discharging 500,000 MT/y) needed to discharge the stated annual treatment volume to the plant.

Treatment System	Number of Ships	Capital Costs			Operating Cost	Annualized Cost
		Storage	Treatment	Ship Retrofit	/1000 MT	/1000 MT
Shipboard [1]	1	0	2,040,844	0	82	529
On-land [2]	11	3,061,266	6,122,532	2,244,928	92	227
On-land [3]	11	6,122,532	6,122,532	2,244,928	92	263
On-land [4]	11	3,061,266	16,326,752	2,244,928	92	348
Treatment ship [5]	14	8,673,587	12,755,275	2,857,182	422	700
Treatment ship [6]	23	8,673,587	12,755,275	4,693,941	276	458
[1] Treating 500,000 MT/y, or about 1 voyage/month.						
[2] Treating 5,500,000 MT/y, with 52,000 MT storage in earthen basins and 830 MT/h treatment rate.						
[3] Treating 5,500,000 MT/y, with 52,000 MT storage in steel tanks and 830 MT/h treatment rate.						
[4] Treating 5,500,000 MT/y, with 4,000 MT storage in steel tanks and 4,000 MT/h treatment rate.						
[5] Treating ≈3 ships/week (described as 40% utilization in AQIS 1993a), or 7,000,000 MT/y.						
[6] Treating ≈5 ships/week (described as 70% utilization in AQIS 1993a), or 11,500,000 MT/y.						

AQIS (1993a) also developed a scenario for onshore treatment of all the ballast water discharged in Australia (estimated at 66 million MT/y from at least 1,000 distinct ships) that included 3 treatment ships and 18 on-land treatment plants located in Australia's major ports, along with 16 barges to transport ballast water collected at smaller ports. The estimated total costs based on these assumptions are shown in Table A1-3. In this scenario the average annual ballast water discharge per ship is much smaller than in the single port scenario of Table A1-2, and the annualized costs per 1,000 MT are therefore larger. In this countrywide scenario, total shipboard treatment costs are about 4.4 times the total treatment costs onshore.

¹⁷ Based on the estimated retrofit cost for a large bulk carrier (AQIS 1993a at p. 73) of \$204,084 in June 2010 US dollars.

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Table A1-3. Treatment cost estimates for shipboard and onshore approaches - Australia-wide scenario (AQIS 1993a). The figures have been adjusted to June 2010 US dollars and annualized as described in Appendix 2.

Approach	Capital Costs			Shipboard Treatment or Retrofit	Operating Cost /1000 MT	Total Annualized Cost
	Onshore Treatment Plants	Treatment Ships	Barges			
Shipboard	—	—	—	2,040,844,000	82	228,879,179
Onshore	183,675,960	61,225,320	81,633,760	204,084,400	102	51,737,298

The study concluded that “land-based or port-based [=treatment ship] facilities are more economic and effective than numerous ship-board plants.” In these estimates, some significant costs (pipes to transport ballast water from berths to treatment plants, and land costs) were not included in the onshore alternatives which reduced their estimated total cost relative to the shipboard alternative. On the other hand, the onshore treatment approach (using granular filtration with coagulation and flocculation followed by UV disinfection) would treat ballast water to a substantially higher standard than the shipboard alternative (using only a 50 µm strainer with no disinfection); and for the single-port scenario, basing the analysis on large bulk carriers, which typically discharge the largest volumes of ballast water of the vessels using Australia’s ports (Table 4.1 in AQIS 1993a), greatly favored shipboard treatment. The estimates are also somewhat sensitive to other factors, including the assumed utilization rates for the onshore systems, and the interest rate used to annualize costs.

In a second study conducted for the Canadian Coast Guard, Aquatic Sciences (1996) considered onshore treatment alternatives (referred to as “pump off options”) for Great Lakes shipping and found them to be “technically feasible” and to “undoubtedly offer the best assurance of prevention of unwanted introductions.” The report further found that when installed onshore, “treatment options could have a more practical and enforceable application” than in shipboard installations, and concluded that “ship board treatment of ballast water appears to be logistically, economically, and particularly from the aspect of control, the least attractive method of ballast water treatment.” The report estimated that treatment ships could be provided at key ports throughout the Great Lakes to receive discharged ballast water and heat it to >65°C at an annualized cost of around \$17 million to (more likely) \$51 million, or alternately a single treatment ship could operate at a site en route to the Great Lakes to treat all incoming ballast water at a annualized cost of \$2.7-2.8 million. Retrofitting costs to enable ships to discharge their ballast water to treatment ships could range from around \$40,000 to over \$200,000 per ship.¹⁸

¹⁸ The costs cited in this paragraph were adjusted to June 1, 2010 US dollars as described in Appendix 1.

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1
2 California's State Water Resources Control Board (California SWRCB 2002) conducted a
3 qualitative evaluation of onshore treatment and ten shipboard treatment alternatives in terms of
4 effectiveness, safety, and environmental acceptability. Onshore treatment was the only approach
5 to be rated acceptable in all three categories. There were reservations or unresolved questions
6 about the effectiveness of all of the shipboard alternatives, about the safety of eight of the
7 shipboard alternatives, and about the environmental acceptability of nine of the shipboard
8 approaches.
9

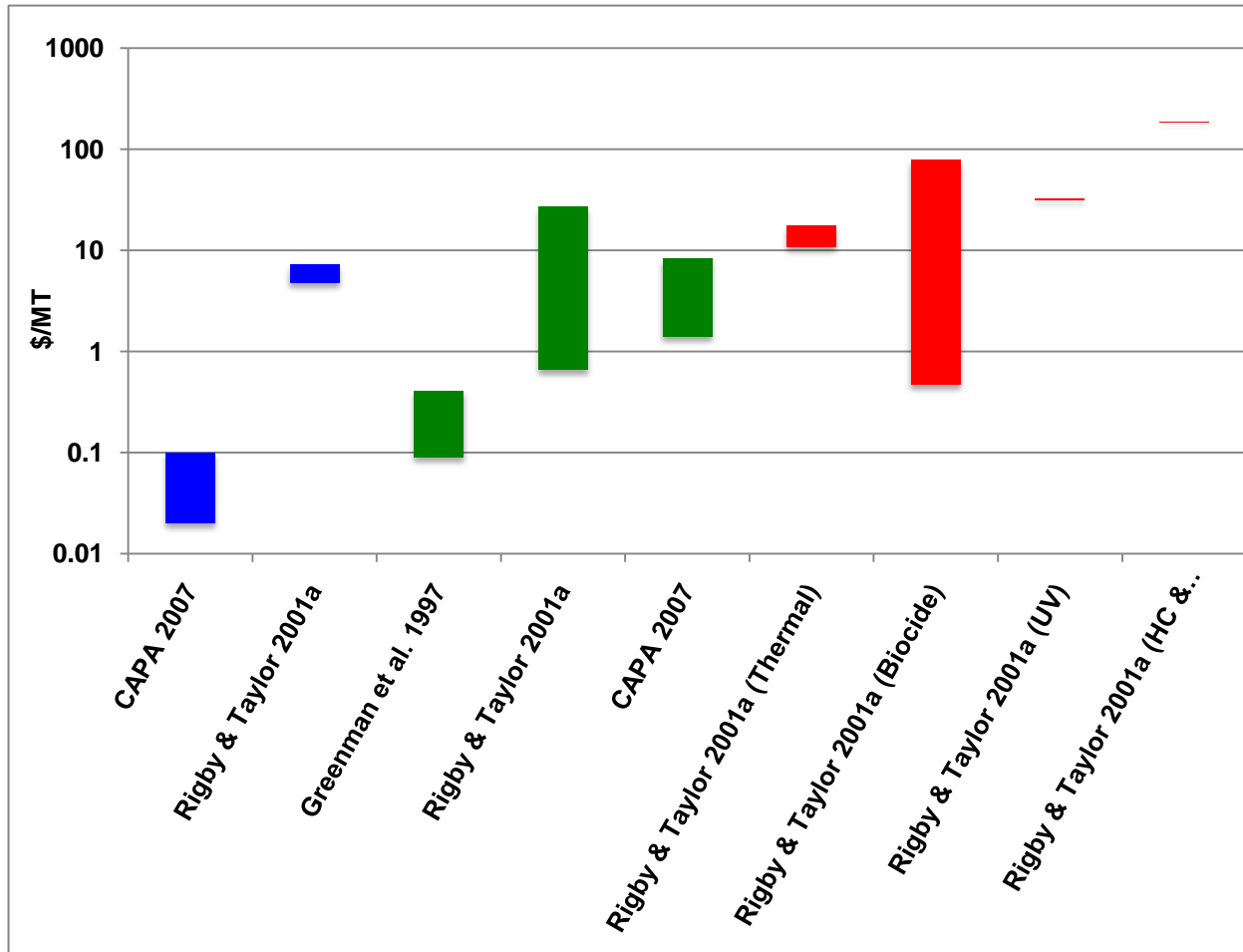
10 In each of these studies, onshore treatment was judged to be as effective or more effective, and
11 generally cheaper, than shipboard treatment. As noted, there are limitations to these studies and
12 grounds for criticism, however the first three appear to be the most detailed comparisons of
13 onshore and shipboard treatment approaches available. In addition, the U.S. Coast Guard
14 compiled a table of cost estimates from different studies for public review and comment (U.S.
15 Coast Guard 2002). Figure A1-1 shows all the estimates that were expressed in the table as costs
16 per metric ton or cubic meter of ballast water, and thus in a form that can be compared. In these
17 estimates, onshore treatment is generally more expensive than ballast water exchange and less
18 expensive than shipboard treatment, though there is considerable overlap.
19
20

21 **Figure A1-1. Cost estimates listed in U.S. Coast Guard (2002).** The Coast Guard converted Australian estimates
22 to U.S. dollars at the Oct. 16, 2001 exchange rate, but did not adjust estimates for inflation. Cost estimates for ballast
23 water exchange are in blue, for onshore treatment in green, and for shipboard treatment in red.
24

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4



The other comparisons of onshore and shipboard treatment in the literature consist of lists or brief discussions of their relative merits. These reports variously conclude that onshore treatment is probably a superior or probably an inferior option compared to shipboard treatment, or that onshore treatment is suitable for a particular part of the cargo fleet (Table A1-1), but none provide any significant analysis or data to support these conclusions.

Two studies (in addition to AQIS (1993a) and Aquatic Sciences (1996), discussed above) provide conceptual designs and cost estimates for onshore treatment for specific regions. CAPA (2000) is an EPA-funded study conducted for the California Association of Port Authorities. This study developed conceptual designs and cost estimates for constructing and operating ballast water treatment plants at each cargo port in California. These plans and estimates include the piping from berths to plants; storage tanks; coagulation, flocculation, filtration and UV

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

disinfection; thickening, dewatering and land-fill disposal of residual solids; and discharge of effluent through an outfall pipeline; they did not include land costs, permitting, seismic evaluation, or costs to retrofit vessels to enable them to discharge ballast water to an onshore facility. The study concluded that onshore treatment would be technically and operationally feasible, though there could be delays to some vessels in some circumstances. The estimated costs are shown in Table A1-4.

Table A1-4. Cost estimates for onshore treatment in California (CAPA 2000). The figures have been adjusted to June 1, 2010 US dollars and annualized as described in Appendix 2.

Port	Capital Costs				Annual O&M	Annualized Costs
	Pipes	Storage Tanks	Treatment Plant	Outfall		
Hueneme [1]	1,325,069	69,014	0	125,480	0	98,850
Humboldt Bay	15,900,826	5,019,200	2,234,799	125,480	187,969	1,702,386
Long Beach	35,909,364	6,399,480	2,786,158	125,480	280,390	3,222,047
Los Angeles	33,921,761	25,597,920	2,786,158	125,480	280,390	4,341,637
Oakland	19,876,032	4,768,240	2,234,799	125,480	187,969	1,944,654
Redwood City	1,987,603	5,395,640	2,047,206	125,480	178,684	800,310
Richmond	7,287,878	4,266,320	2,047,206	125,480	178,684	1,071,637
Sacramento	1,722,589	6,023,040	2,047,206	125,480	178,684	823,884
San Diego	11,660,605	3,889,880	2,047,206	125,480	178,684	1,331,601
San Francisco	10,600,550	7,905,240	2,234,799	125,480	187,969	1,545,337
Stockton	6,757,851	6,901,400	2,047,206	125,480	178,684	1,208,574
California	146,950,130	76,235,374	22,512,743	1,380,280	2,018,105	18,090,918
[1] CAPA (2000) concluded that building a treatment plant at Port Hueneme made no sense because so little ballast was discharged there (<2 MT/d), and that instead the ballast water could be “discharged to the sewer, reballasted to an outgoing ship, taken to another port for treatment,...transported by a separate vessel for discharge at sea” or batch treated with chlorine. The report estimated piping, storage and outfall costs for this site, but did not estimate treatment plant costs.						

Brown and Caldwell (2007, 2008) developed designs and cost estimates for on-land and treatment ship approaches to treating the ballast discharges from oceangoing ships arriving at the Port of Milwaukee. The first report assessed four on-land treatment systems:

- 100-µm screening followed by UV treatment;
- coarse screening followed by ozonation;
- 500-µm screening followed by membrane filtration to remove particles >0.1 µm;
- 500-µm screening followed by hydrodynamic cavitation.

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

These were each analyzed along with two systems for transferring and storing the discharged ballast water: discharge at berths into pipes that carry the water to on-land storage tanks and a treatment plant; and discharge to a barge that stores the water and carries it to an on-land treatment plant. Design criteria assumed 85 ship arrivals during the eight months that the St. Lawrence Seaway is open each year, and a system capable of receiving ballast water at 680 MT/h, with storage capacity of 1,900 MT, and treatment at 80 MT/h. Estimated costs are shown in Table A1-5. The report concluded that all four treatment systems and both transport/storage systems are feasible, with UV treatment and hydrodynamic cavitation having the most promise for treating viruses (Brown and Caldwell 2007). The second report (Brown and Caldwell 2008) developed a design and cost estimate for retrofitting a barge to serve as a treatment ship, which would collect, store and treat ballast water. The treatment system included a cloth media disk filter with a nominal pore size of 10 µm, and UV treatment at an estimated minimum dose of 30 mJ/cm². The design criteria for this analysis required the capacity to receive ballast discharges at 2,300 MT/h, storage of 10,000 MT, and treatment at 230 MT/h, thus around 3 times the flow rates and 5 times the storage required in the first report. The cost estimates for the eight on-land treatment alternatives analyzed in the first report, adjusted to meet the more demanding design criteria used in the second report, plus the cost estimates for the treatment ship in the second report, are shown in Table A1-6.

Table A1-5. Cost estimates for onshore treatment for oceangoing ships at the Port of Milwaukee (Brown and Caldwell 2007). The figures have been adjusted to June 1, 2010 US dollars and annualized as described in Appendix 2.

Treatment (Transport) [1]	— Pipes [2]	Capital Costs Storage	— Treatment	Annual O&M	Annualized Costs
100-µm screening & UV (pipes)	2,973,120	1,251,840	584,192	13,986	399,885
Ozone (pipes)	2,973,120	1,251,840	834,560	9,806	415,795
0.1-µm membrane filter (pipes)	2,973,120	1,251,840	1,043,200	19,917	442,648
Hydrodynamic cavitation (pipes)	2,973,120	1,251,840	2,608,000	20,864	569,158
100-µm screening & UV (barge) [3]	260,800	521,600	584,192	369,166	478,825
Ozone (barge) [3]	260,800	521,600	834,560	364,985	494,734
0.1-µm membrane filter (barge) [3]	260,800	521,600	1,043,200	375,096	521,587
Hydrodynamic cavitation (barge) [3]	260,800	521,600	2,608,000	376,043	648,098

[1] Design criteria are: maximum ballast discharge of 680 MT/h, storage of 1,900 MT, and treatment rate of 80 MT/h; “(pipes)” refers to discharge of ballast water at berths into a pipe system connecting to the treatment plant; “(barge)” refers to discharge to a barge to transport the ballast water to the treatment plant.

[2] Includes collection pumps, pipes and a lift/coarse screening station.

[3] "Storage" refers to barge purchase and modification costs for use as transfer and storage vessel, exclusive of treatment system.

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Table A1-6. Cost estimates for onshore treatment for oceangoing ships at the Port of Milwaukee (Brown and Caldwell 2007, 2008). The figures for the eight alternatives analyzed in Brown and Caldwell (2007) have been adjusted to meet the design criteria of Brown and Caldwell (2008) as described in Appendix 3. All figures have been adjusted to June 1, 2010 US dollars and annualized as described in Appendix 2.

Treatment (Transport) [1]	— Pipes [2]	Capital Costs — Storage	— Treatment	Annual O&M	Annualized Costs
100-µm screening & UV (pipes)	5,384,924	3,546,880	1,669,120	13,986	864,632
Ozone (pipes)	5,384,924	3,546,880	2,384,457	9,806	917,852
0.1-µm membrane filter (pipes)	5,384,924	3,546,880	2,980,571	19,917	975,797
Hydrodynamic cavitation (pipes)	5,384,924	3,546,880	7,421,623	20,864	1,333,105
100-µm screening & UV (barge) [3]	794,819	1,043,200	1,669,120	369,166	650,588
Ozone (barge) [3]	794,819	1,043,200	2,384,457	364,985	703,808
0.1-µm membrane filter (barge) [3]	794,819	1,043,200	2,980,571	375,096	761,753
Hydrodynamic cavitation (barge) [3]	794,819	1,043,200	7,421,623	376,043	1,119,061
10-µm filter & UV (treatment ship) [3]	0	2,695,184	808,854	518,914	800,087
[1] Design criteria are: maximum ballast discharge of 2,300 MT/h, storage of 10,000 MT, and treatment rate of 230 MT/h; “(pipes)” refers to discharge of ballast water at berths into a pipe system connecting to the treatment plant; “(barge)” refers to discharge to a barge to transport the ballast water to the treatment plant.					
[2] Includes collection pumps, pipes and a lift/coarse screening station.					
[3] "Storage" refers to barge purchase and modification costs for use as transfer and storage vessel or as treatment ship, exclusive of treatment system.					

Besides the need for facilities to receive and transport ballast water from ships, store it and treat it, ships must be modified so they can safely and rapidly discharge ballast water to onshore facilities. There have been several estimates of the costs of these retrofits (Table A1-7), which require modifications in a ship’s pipe system and may require the installation of larger ballast pumps (in order to raise the water to deck level, and/or to discharge it quickly enough). These costs may vary between different types and sizes of ships, with the costs ranging from around \$15,000 to \$540,000 for container ships (Pollutech 1992; Glosten 2002), from around \$15,000 to \$500,000 for bulkers (Pollutech 1992; CAPA 2000), and from considerably less than \$140,000 to around \$2.3 million for tankers (Victoria ENRC 1997; Glosten 2002) (Fig. A1-2). Most of these estimates specifically included costs for replacing existing pumps with more powerful pumps where needed (AQIS 1993a; Aquatic Sciences 1996; Dames & Moore 1998; CAPA 2000; Glosten 2002¹⁹; Brown and Caldwell 2008²⁰). The estimated cost to outfit a new ship would be

¹⁹ Glosten (2002) designed the pumps and pipe systems to be large enough to enable ships to deballast completely at berth during a typical cargo loading period.

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

less than the cost to retrofit a comparable existing ship (AQIS 1993b), perhaps by as much as an order of magnitude (CAPA 2000).

Table A1-7. Cost estimates for retrofitting ships to discharge ballast water to a treatment facility. The figures have been adjusted to June 1, 2010 US dollars as described in Appendix 2. In the parentheses following the ship type, length is given in feet, size in deadweight tons (DWT), ballast water capacity in metric tons (MT), and maximum ballast discharge rate in metric tons per hour (MT/h), if stated.

Ship Type	Capital Cost	Report
Great Lakes bulker, break-bulk or container	\$13,233–26,465	Pollutech 1992
Small container	\$20,408	AQIS 1993a
Large bulker (140,000 DWT; 45,000 MT; 4,000 MT/h)	\$204,084	AQIS 1993a
Great Lakes bulker	\$40,352–201,758	Aquatic Sciences 1996
Handysize bulker (520'; 22,000 DWT)	\$142,340	Victoria ENRC 1997
Container	\$53,196–172,887	Dames & Moore 1998 [1]
Container or bulker (1,000 MT/h)	\$501,920	CAPA 2000
Tanker (869'; 123,000 DWT; 75,850 MT; 6,400 MT/h)	\$2,328,607	Glosten 2002
Bulker (735'; 67,550 DWT; 35,000 MT; 2,600 MT/h)	\$131,316	Glosten 2002
Break-bulk (644'; 40,300 DWT; 26,850 MT; 3,000 MT/h)	\$373,394	Glosten 2002
Container (906'; 65,480 DWT; 19,670 MT; 2,000 MT/h)	\$539,539	Glosten 2002
Car carrier (570'; 13,847 DWT; 6,600 MT; 550 MT/h)	\$197,773	Glosten 2002
Bulker (469'; 5,700 MT; 570 MT/h)	\$59,694	Brown and Caldwell 2008
Bulker (722'; 18,000 MT; 2,300 MT/h)	\$202,960	Brown and Caldwell 2008
[1] Estimate developed by the Pacific Merchant Shipping Association.		

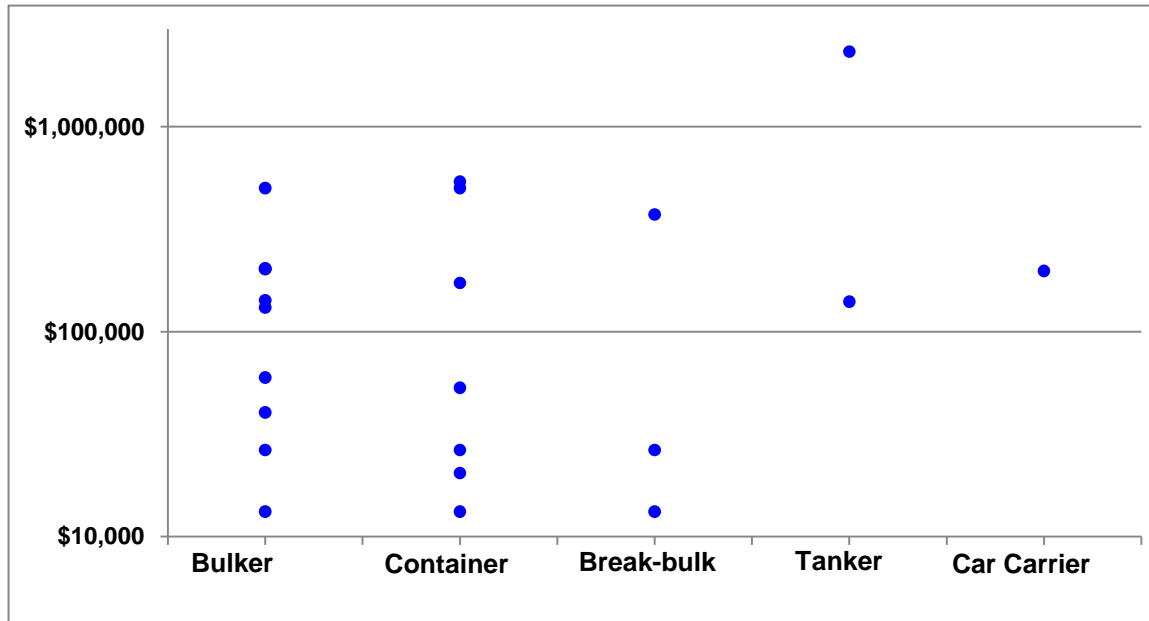
Figure A1-2. Cost estimates for retrofitting ships to discharge ballast water to a treatment facility. The figures have been adjusted to June 2010 US dollars as described in Appendix 2. Some estimates apply to more than one ship type, and appear in more than one column in the figure.

²⁰ Brown and Caldwell (2008) found, based on pump and pipe system curves (dynamic head vs. flow), that the small and large Great Lakes bulk carriers they analyzed would not need larger ballast pumps—that is, with their existing pumps the ships could fully deballast while at berth during the time it takes to load cargo.

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1
2
3
4 Some of these reports provide little or no supporting data or explanation for the cost estimates
5 (Pollutech 1992; AQIS 1993a; Aquatic Sciences 1996; Dames & Moore 1998). Victoria ENRC
6 (1997) provided a materials list for a bulk carrier, and noted that a tanker “with its ballast lines
7 running on deck would have a considerable lower installation cost.” CAPA (2000) provided a
8 cost-breakdown for modifying a bulk carrier, and stated that modifying a tanker would generally
9 cost more.

10
11 Glosten (2002) and Brown and Caldwell (2008) provided the most recent and most detailed
12 estimates. Glosten (2002) estimated ship modification costs for ballast water transfer systems on
13 five ships representing common types of vessels calling at Puget Sound ports (Table A1-6).
14 These systems were designed to “allow ballast transfer with minimal disruption to current
15 operations,” including sizing them to allow vessels to deballast completely at berth during the
16 time needed to complete cargo loading, thereby eliminating the need to start deballasting before
17 arriving at berth. To represent each vessel category, the authors selected ships that “had ballast
18 systems with capacities on the upper end of vessels that call on Puget Sound to attempt to
19 establish an upper-bound on retrofitting costs.” In addition, in selecting pipe sizing and other
20 design elements, “every attempt was made to capture an upper bound on the modification costs
21 associated with each vessel type surveyed.” This included the installation of “a completely new
22 piping system to provide the ability to fill and empty each ballast tank separately.” Notably, this
23 new piping system was included even though it is not needed on crude oil tankers, the type of
24 tanker analyzed (which produced by far the highest cost estimate in the study), where “a simpler,
25 lower-cost solution” exists, because it might be needed on some other ships (i.e. product tankers)

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 in the same general category.²¹ The transfer systems were also designed to allow ballast water
2 transfer in either direction between a ship and an onshore facility (either onto or off a ship),²²
3 which in some cases may raise the cost over what is needed to only discharge ballast water to
4 onshore facilities.

5
6 Brown and Caldwell (2008) provided analyses, conceptual designs, schematic drawings and cost
7 estimates for modifying two sizes of ocean-going bulk carriers serving the Great Lakes, based a
8 smaller, actual ship and a larger hypothetical ship (Table A1-6). These designs were also sized to
9 allow the ship to initiate and complete deballasting at berth during cargo loading.

10
11 In addition to discussions or analyses of onshore treatment in reports, the potential for treating
12 ballast discharges onshore has been recognized in laws, regulations, guidelines and treaty
13 conventions. The U.S. Nonindigenous Aquatic Nuisance Prevention and Control Act (NANPCA)
14 of 1990 and the National Invasive Species Act (NISA) of 1996 directed the U.S. Coast Guard to
15 fund research on ballast water management, specifically noting that technologies in “land-based
16 ballast water treatment facilities” could be included, and to investigate the feasibility of using or
17 modifying onshore ballast water treatment facilities used by Alaskan oil tankers to reduce the
18 introduction of exotic organisms (§§1101(k)(3), 1104(a)(1)(B), 1104(a)(2) and 1104(b)(3)(A)(ii)
19 in U.S. Congress 1990, 1996). In its interim and final rules implementing NISA, the U.S. Coast
20 Guard specifically included discharge to an onshore treatment facility as a means of meeting
21 NISA’s ballast discharge requirements, and required ships to keep records of ballast water
22 discharged to such facilities (US Coast Guard 1999, 2001), although the Coast Guard eliminated
23 these provisions when it concluded that it did not have the authority to regulate or approve
24 onshore ballast water treatment plants (US Coast Guard 2004). The U.N. International Maritime
25 Organization’s 1991 Guidelines state that “Where adequate shore reception facilities exist,
26 discharge of ship’s ballast water in port into such facilities may provide an acceptable means of
27 control” (IMO 1991 and IMO 1993, §7.5 Shore Reception Facilities). The IMO’s 1997
28 Guidelines state that “Discharge of ship’s ballast water into port reception and/or treatment
29 facilities may provide an acceptable means of control. Port State authorities wishing to utilize
30 this strategy should ensure that the facilities are adequate...If reception facilities for ballast water
31 and/or sediments are provided by a port State, they should, where appropriate, be utilized” (IMO
32 1997, §7.2.2, §9.2.3). The IMO’s 2004 Convention states that “The requirements of this
33 regulation do not apply to ships that discharge ballast water to a reception facility designed
34 taking into account the Guidelines developed by the Organization for such facilities” (IMO 2004,
35 Regulation B-3.6). The IMO adopted specific guidelines for onshore ballast water treatment
36 facilities (IMO 2006), and also recognized onshore treatment as an alternative in IMO 2005b

²¹ This is consistent with the study’s stated aim, to quantify “the capital cost required to provide the maximum capability in a ballast transfer system, to represent a maximum capital investment” for each vessel category (Gloston 2002).

²² The ability to move ballast water onto a ship from an onshore service was included to accommodate the possibility of loading “clean” ballast, an approach that is not considered to be onshore treatment in this report.

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

- 1 (§1.2.3), as do Australia, New Zealand and Canada in their ballast water regulations (AQIS
- 2 1992; New Zealand 1998, 2005; Canada 2000, 2007).

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Appendix 2. Cost Estimate Adjustments and Calculation of Annualized Costs

Estimates made in foreign currencies in the original publications were converted into US dollars at the daily average interbank transfer rates reported at <http://www.oanda.com/currency/historical-rates> on the date of publication or presentation, or on the first day of the month where only the month of publication was given. For the estimates used in this report, the transfer rates are listed in Table A2-1.

Table A2-1. Currency exchange rates used in this report.

Publication	Original Currency	Exchange Date	US Exchange Rate
Pollutech 1992	Canadian dollars	3/31/1992	0.845700
AQIS 1993	Australian dollars	6/1/1993	0.676000
Ogilvie 1995	New Zealand dollars	6/29/1995	0.762266
Aquatic Sciences 1996	Canadian dollars	8/1/1996	0.728000
Victoria ENRC 1997	Australian dollars	10/1/1997	0.727800

Estimates were inflated from the date of original publication, or from the first day of the month where only the month of publication was given, to June 1, 2010 using the calculator at http://inflationdata.com/inflation/Inflation_Calculators/InflationCalculator.asp, which is based on the U.S. Bureau of Labor Statistics' Consumer Price Index for all Urban Consumers (CPI-U).

Total annualized costs were calculated as the sum of the annual operations & maintenance (O&M) costs and the annualized capital costs:

$$A_T = A_{O\&M} + A_C$$

with:

$$A_C = iC / (1 - (1+i)^{-N})$$

where i = the annual interest rate on borrowed capital, C = the capital cost, and N = the working lifetime of the plant or equipment in years. This formula assumes that the entire capital cost is incurred at the start of the project. We assumed an interest rate of 5%, and the following working lifetimes:

New cargo vessel	25 years
Retrofitted cargo vessel	12.5 years

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

- | | | |
|---|-------------------------|----------|
| 1 | Treatment ship | 20 years |
| 2 | On-land treatment plant | 30 years |

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Appendix 3. Adjustment of the Cost Estimates in Brown and Caldwell (2007) to the Design Criteria in Brown and Caldwell (2008)

The design criteria used in the two studies and the ratios between them are shown in Table A3-1. Cost estimates made on the basis of the first set of design criteria were adjusted to reflect the second set of design criteria as described below.

Table A3-1. Design criteria in Brown and Caldwell (2007) and (2008).

Design Criterion	2007 Study	2008 Study	Ratio (2008:2007)
Ballast Discharge Rate (gpm)	3,000	10,000	3.33
Storage (gallons)	500,000	2,700,000	5.40
Treatment Rate (gpm)	350	1,000	2.86

Capital cost of pipes: The cost estimate for pipes from the berths to the treatment plant reflecting the 2008 study's Ballast Discharge Rate was interpolated from the values in Table 4 in Brown and Caldwell (2007). This cost estimate is 1.7 times the estimate in Brown and Caldwell (2007) based on the 2007 study's Ballast Discharge Rate.

Capital cost for on-land storage tanks: This estimate was taken from Table 6 in Brown and Caldwell (2007) for 3 million gallons of storage (2.7 million gallons of storage is required). This cost estimate is 2.8 times the estimate in Brown and Caldwell (2007) based on the 2007 study's Storage requirement.

Capital cost for barge purchase and modification: This was estimated as the cost of two barges, since one barge has a storage capacity of 1,700,000 gallons (Brown and Caldwell 2007 at p. 15) and 2,700,000 gallons of storage is needed. This value is thus double the estimate in Brown and Caldwell (2007) based on the 2007 study's Storage requirement.

Capital cost for collection pumps: The governing criterion is the Ballast Discharge Rate, which is 3.33 times higher in the 2008 study than in the 2007 study. Other capital costs show substantial economies of scale, that is, the ratio of estimated costs is less than the ratio of design criteria (Table A3-2). To reflect economies of scale, the estimated cost for collection pumps was increased by 1.7 relative to the estimate in Brown and Caldwell (2007), which is based on the 2007 study's Ballast Discharge Rate.

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 **Table A3-2. Comparison of criteria and cost estimate ratios for pipe, storage and barge estimates.**
2

Estimated Cost	Governing Criterion	Ratio of Criteria	Ratio of Cost Estimates
Pipes	Ballast Discharge Rate	3.33	1.7
Storage Tanks	Storage	5.40	2.8
Barge	Storage	5.40	2.0

3
4
5 *Capital cost for lift station:* The governing criterion is the Treatment Rate, which is 2.86 times
6 higher in the 2008 study than in the 2007 study. As with the estimated capital cost for collection
7 pumps, in order to reflect economies of scale the estimated cost for the lift station was increased
8 by 1.7 relative to the estimate in Brown and Caldwell (2007) based on the 2007 study's
9 Treatment Rate.

10
11 *Capital costs for treatment systems:* For Filtration & UV, Ozonation, and Membrane Filtration,
12 the governing criterion is the Treatment Rate, which is 2.86 times higher in the 2008 study than
13 in the 2007 study. For these systems, as with other capital costs whose size is governed by flow
14 rates, in order to reflect economies of scale the estimated cost was increased by 1.7 relative to the
15 estimates in Brown and Caldwell (2007) based on the 2007 study's Treatment Rate.

16
17 For Hydrodynamic Cavitation, part of the capital cost is to provide additional storage. This part
18 of the cost was estimated from Table 6 in Brown and Caldwell (2007) for 3 million gallons of
19 storage (2.7 million gallons of storage is required). For the remaining part of the capital cost, as
20 with other capital costs whose size is governed by flow rates, in order to reflect economies of
21 scale the estimated cost was increased by 1.7 relative to the estimates in Brown and Caldwell
22 (2007) based on the 2007 study's Treatment Rate.

23
24 *Barge O&M:* These costs are for towing services, which are based on the number of ship arrivals
25 per year. This number did not change between the two studies, so this cost estimate was not
26 changed.

27
28 *Treatment system O&M:* These costs, and equipment replacement costs which are here included
29 under O&M, appear to be based on the total annual volume of ballast water discharged. This
30 does not appear to change between the two studies, so this cost estimate was not changed.

31
32 Two sensitivity analyses were conducted to assess the above assumptions. If the capital costs for
33 collection pumps, lift stations and treatment systems are increased proportional to the governing
34 criteria (Ballast Discharge Rate or Treatment Rate) rather than by a factor of 1.7 (i.e. if we
35 assume that there are no economies of scale in the capital costs for these system components),
36 the cost estimates for the various systems increase by 9-19%. If Treatment system O&M costs
37 are increased proportional to the governing criterion (Treatment Rate) rather than not increased,

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

- 1 the cost estimates for the various systems increase by 3-6%. The adjustments in the cost
- 2 estimates thus seem fairly robust relative to these assumptions.
- 3

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Appendix 4. Estimates of Treatment Plants and Capacities in Onshore and Shipboard Treatment Approaches for Milwaukee, Australia, California and the United States

Shipboard ballast water treatment systems must generally be sized large enough to accommodate the maximum ballast pumping capacities of the ships they are installed on (Table A4-1). This requires some very large-capacity treatment plants—in the largest vessels, the required 20,000 MT/h capacity is greater than the estimated wastewater treatment capacity needed to serve the population of Phoenix, Arizona, the fifth largest city in the United States (Table A4-2). In contrast, onshore ballast treatment plants with adequate storage need only be large enough to treat at the average (not the maximum) ballast discharge rate. This results in a large difference in the required treatment capacity in shipboard and onshore approaches.

Table A4-1. Ships' total ballast pump capacities. The total ballast pump capacity is the summed capacities of all ballast pumps that can operate simultaneously.

Vessel Type	Typical Total Ballast Pump Capacity (MT/h)	Reference
Containerships	250-750	ABS 2010
Australian Containerships	500-2,000	AQIS 1993a
Containerships	1,100	Rigby & Taylor 2001b
Containerships	1,000-2,000	NRC 1996
Japan-Oregon Woodchip Carriers	780-975	Carlton et al. 1995
Australian Woodchip Carriers	1,000-1,500	AQIS 1993a
Bulk Carriers	1,300-3,000	ABS 2010
Australian Bulk Carriers	1,000-6,000	AQIS 1993a
Capesize Bulk Carriers	6,000	Rigby & Taylor 2001b
Bulk Carriers	2,000-10,000	Reeves 1999
Bulk Carriers, Ore Carriers	5,000-10,000	NRC 1996
Largest Bulk Carriers	to >20,000	AQIS 199a
Australian Tankers	750-3,000	AQIS 1993a
Tankers	1,100-5,800	ABS 2010
LNG Tanker	6,000	Rigby & Taylor 2001b
Tankers	5,000-20,000	NRC 1996; Reeves 1999
Largest Tankers	to >20,000	AQIS 199a

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

New Zealand ships	1,000-1,500	Ogilvie 1999
Great Lakes ships	550-3,500	Brown and Caldwell 2008
Great Lakes ships	400-5,000	Pollutech 1992
Great Lakes ships	2,000-5,900	Aquatic Sciences 1996
Largest vessels	15,000-20,000	NRC 1996

Table A4-2. Estimated wastewater treatment capacities needed to serve the populations of selected US cities.

Based on July 1, 2008 populations (U.S. Census 2010) and the average per capita domestic wastewater production in North America (UNEP 2000). Rank is the rank among U.S. cities in population.

Treatment Capacity (MT/h)	City	Population	Rank
16,987	Phoenix AZ	1,568,000	5
4,897	Kansas City MO	452,000	39
4,702	Cleveland OH	434,000	41
4,474	Miami FL	413,000	43
1,972	Salt Lake City UT	182,000	125
1,495	Syracuse NY	138,000	174
1,387	Cedar Rapids IA	128,000	187
1,343	Hartford CT	124,000	193

The treatment plant and treatment capacity needed for onshore treatment in the Port of Milwaukee, Australia and California were estimated based on conceptual design studies of onshore treatment in those locations (with various adjustments described below). The estimate for the U.S. was based on the California estimate adjusted to reflect the larger amount of ballast water that is discharged in the U.S. The shipboard treatment estimates were based on the estimated number of distinct ships arriving or discharging ballast in these locations (for the number of treatment plants), multiplied by the average ballast pump capacity of these ships (for the treatment capacity). For sites with onshore studies that include on-land treatment plants, the project period for the estimate is 30 years based on the estimated useful life of an on-land treatment plant (Appendix 2). For the onshore study based on a treatment ship only (Brown and Caldwell 2008), the project period for the estimate is 20 years. For each site, the estimated number of affected ships for the shipboard estimate was based on these project periods, adjusted to reflect the estimated 25-year useful life of a ship.

In each of these estimates, adjustments were selected that are *conservative* in the sense of tending to produce a smaller shipboard:onsshore ratio for treatment plants or treatment capacity, which is the sense in which the word is used below. That is, as used in this Appendix, conservative

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

adjustments are those that tend to raise the number of treatment plants or the total treatment capacity needed for onshore treatment, or to lower those numbers for shipboard treatment.

Port of Milwaukee (overseas ships only)

Onshore estimate: Brown and Caldwell (2008) estimated that a single ballast water treatment ship with a maximum treatment rate of 230 MT/h could serve the overseas ships calling at the Port of Milwaukee.

Shipboard estimate, number of treatment plants: About 85 overseas ships call at the port each year during the 8 months that the St. Lawrence Seaway is open (Brown and Caldwell 2008). Assuming that each roundtrip voyage takes a month, this would require a minimum of 11 different overseas cargo ships to visit the port during the first year. Over the remaining 19 years of the 20-year period of the estimate (corresponding to the estimated useful working life a treatment ship), other overseas cargo ships would call at the Port consisting of a combination of (a) new ships that come into service to replace ships that had called at the Port during the first year, and (b) other ships, including other new ships and old ships that hadn't called at the Port during the first year. With a typical useful working life for a cargo ship of 25 years, approximately 19/25 of the ships calling at the Port in the first year will go out of service and be replaced by other vessels during the remainder of the 20-year period. Since raising the number of ships raises the number of treatment plants and the total treatment capacity that would need to be installed to accommodate shipboard treatment, we conservatively adjust the number of ships by counting only the additional ships that call as replacements for the ships that called during the first year, and ignoring other ships. The estimated number of distinct ships, and of treatment plants needed, is thus 19 ($= 11 \times (1 + 19/25)$).

Shipboard estimate, treatment capacity: In describing ships at the Port of Milwaukee, Brown and Caldwell (2008) state that "typically, cargo ships have two to three pumps that pump the ballast water to one of the various discharge locations on the ship...In general, each of the pumps within the ballast water tanks has a capacity that ranges from 1,000 gpm to 5,000 gpm, and often two of the pumps operate simultaneously." Thus, these ships typically have ballast pump capacities of 2,000 gpm (≈ 450 MT/h) to 10,000-15,000 gpm ($\approx 2,300$ -3,400 MT/h). For the estimate, we assumed an average capacity of 1,200 MT/h. With 19 distinct ships, the total treatment capacity that will need to be installed is 22,800 MT/h.

Australia

Onshore estimate: AQIS (1993a) estimated that Australia's domestic and foreign ballast discharges could be treated with 3 treatment ships and 18 on-land treatment plants located in Australia's major ports, along with 16 barges to transport ballast water collected at smaller ports. Since the estimated working lives are 20 years for a treatment ship and 30 years for an on-land

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 plant, a 30-year period was used for the estimate and the number of treatment ships required was
2 increased to 5. This is a conservative adjustment, since the calculated need over 30 years is for
3 only 4.5 treatment ships. The total treatment capacity of the 18 on-land plants and 5 treatment
4 ships is 34,940 MT/h.

5
6 *Shipboard estimate:* AQIS (1993a, pp. 86, 88) reported that at least 1,000 different ships visit
7 Australian ports each year, discharging 66 million MT of ballast water. If each of these ships
8 discharges its entire typical ballast load into Australian waters once a month, the typical ballast
9 load would be 5,500 MT. Data on Australian ships shows that ballast pump capacities are about
10 10% of typical ballast loads (AQIS 1993a, Table 4.1), thus the average ballast pump capacity for
11 Australian vessels is estimated to be 550 MT/h. This is almost certainly a substantially
12 conservative estimate, since AQIS (1993a, Table 4.1) lists typical ballast pump capacities for
13 ships in Australia ranging from 500 MT/h (for small containerships) to 6,000 MT/h (for large
14 bulk carriers), with an unweighted average for different ship types of 2,089 MT/h. Using a higher
15 estimate of average ballast pump capacity would produce a correspondingly higher estimate of
16 the total treatment capacity needed.

17
18 Adjusting the ship numbers to a 30-year period by adding only the expected number of
19 replacement ships (and ignoring other ships, a conservative adjustment) yields 2,160 distinct
20 ships requiring 2,160 treatment plants. With an average ballast pump capacity of 550 MT/h, a
21 total treatment capacity of over one million MT/h would need to be installed.

22
23 California

24
25 *Onshore estimate:* CAPA (2000) estimated that 10 on-land treatment plants (one at each of ten
26 ports) with a total treatment capacity of 489 MT/h could treat the ballast water discharged into
27 California waters. However, the port descriptions in this study suggested that it would be more
28 economically efficient to serve some of the ports with a few smaller treatment plants rather than
29 a single larger one, so we instead estimated that a total of 16 onshore plants are needed.

30
31 The conceptual design in CAPA (2000) provided sufficient storage at each site to allow the
32 plants to treat the ballast water at the average rate of discharge. However, the study developed
33 designs and cost estimates for only a few sizes of treatment plant, and allocated to each port the
34 next size of plant that was greater than the average ballast discharge at that port. In some cases
35 these plants were nearly 50% larger than needed, resulting in an estimate of total treatment
36 capacity needed in the state (489 MT/h) that is nearly 30% higher than the average rate of
37 discharge in the state (377 MT/h). We conservatively based our estimate on the inflated estimate
38 used in the CAPA (2000) report.

39
40 The estimates in CAPA (2000) were based on some of the earliest ballast discharge data
41 collected by the U.S. Coast Guard or the State of California, which covered less than a year at

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

the time of the study, only included data from ships that had traveled overseas, and suffered from low reporting rates. CAPA (2000) corrected for the time period (that is, annualized the data) but not for the other data limitations. We utilized the most recent available report from the National Ballast Information Clearinghouse summarizing U.S. Coast Guard ballast water data (Miller et al. 2007, covering data for 2004-2005), adjusted these data for reporting rates aggregated by Captain of the Port Zones (COPTZ) in California, and summed these for both foreign and domestic ballast water to estimate total ballast discharge in California (Table A4-3). We then adjusted the treatment capacity estimate from CAPA (2000) by the ratio between the estimate that we derived for California discharge from the Miller et al. (2007) data (12,251,089 MT/y, see table below) and the CAPA (2000) estimate for California discharge (3,302,988 MT/y, summed from Table 5.2 in CAPA (2000)), yielding an estimate of 1,814 MT/h of onshore treatment capacity needed in California (or nearly 4 times the estimate in CAPA (2000)).

Table A4-3. Estimate of the total annual ballast water discharge into California waters (metric tons).

	Domestic			Foreign			Total
	Reported Discharge	Reporting Rate	Estimated Discharge	Reported Discharge	Reporting Rate	Estimated Discharge	Estimated Discharge
Source:	Table 8	Table 4		Table 6	Table 3		
DATA FOR 2004-2005							
SFCMS	4,379,050	104.8	4,178,483	2,975,652	73.7	4,037,520	8,216,003
LOSMS	4,612,242	78.6	5,867,992	5,741,283	98.4	5,834,637	11,702,629
SDCMS	3,452,378	77.7	4,443,215	112,825	80.4	140,330	4,583,545
California			14,489,690			10,012,487	24,502,177
ANNUAL DATA							
California			7,244,845			5,006,244	12,251,089
Source is the table in Miller et al. 2007 from which the data were taken. Captain of the Port Zones are: SFCMS = San Francisco; LOSMS = Los Angeles-Long Beach; SDCMS = San Diego							

Shipboard estimate, number of treatment plants: Figure A4-1 below shows the estimated cumulative number of distinct ships arriving at California ports since January 1, 2000, based on data provided by the California State Lands Commission or contained in California SLC (2010). It's not clear whether the data for the first 4.5 years includes ships on coastal voyages, since such ships were not required to file ballast water report forms during that time; if these are not included, Figure A4-1 could substantially underestimate the number of distinct ships. A total of 7,327 distinct ships were recorded through March 31, 2010, a period of 10.25 years. Adjusting the ship numbers for the 30-year period by adding only the expected number of replacement ships (a conservative adjustment) yields 13,115 distinct ships expected to be subject to ballast

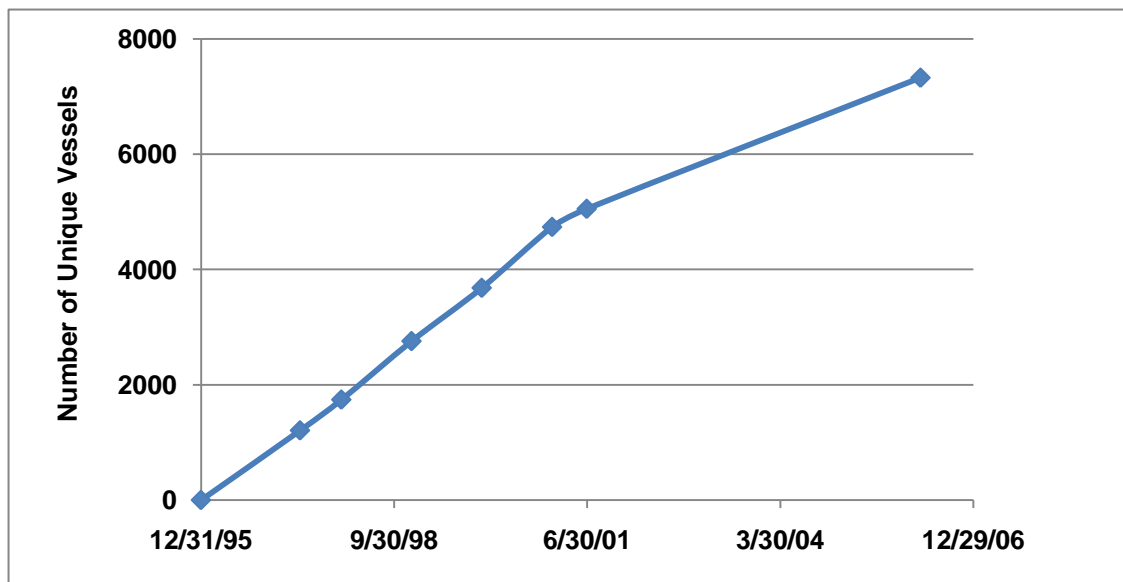
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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

water regulations, potentially requiring 13,115 treatment plants. However, not all arriving ships discharge ballast water, so it's not clear whether all of these ships would need a treatment plant installed. This is discussed further below under the estimate of shipboard treatment capacity.

Figure A4-1. Cumulative number of unique ships arriving at California ports since January 1, 2000. Includes a small number of unmanned barges (a total of 28 through June 2005).



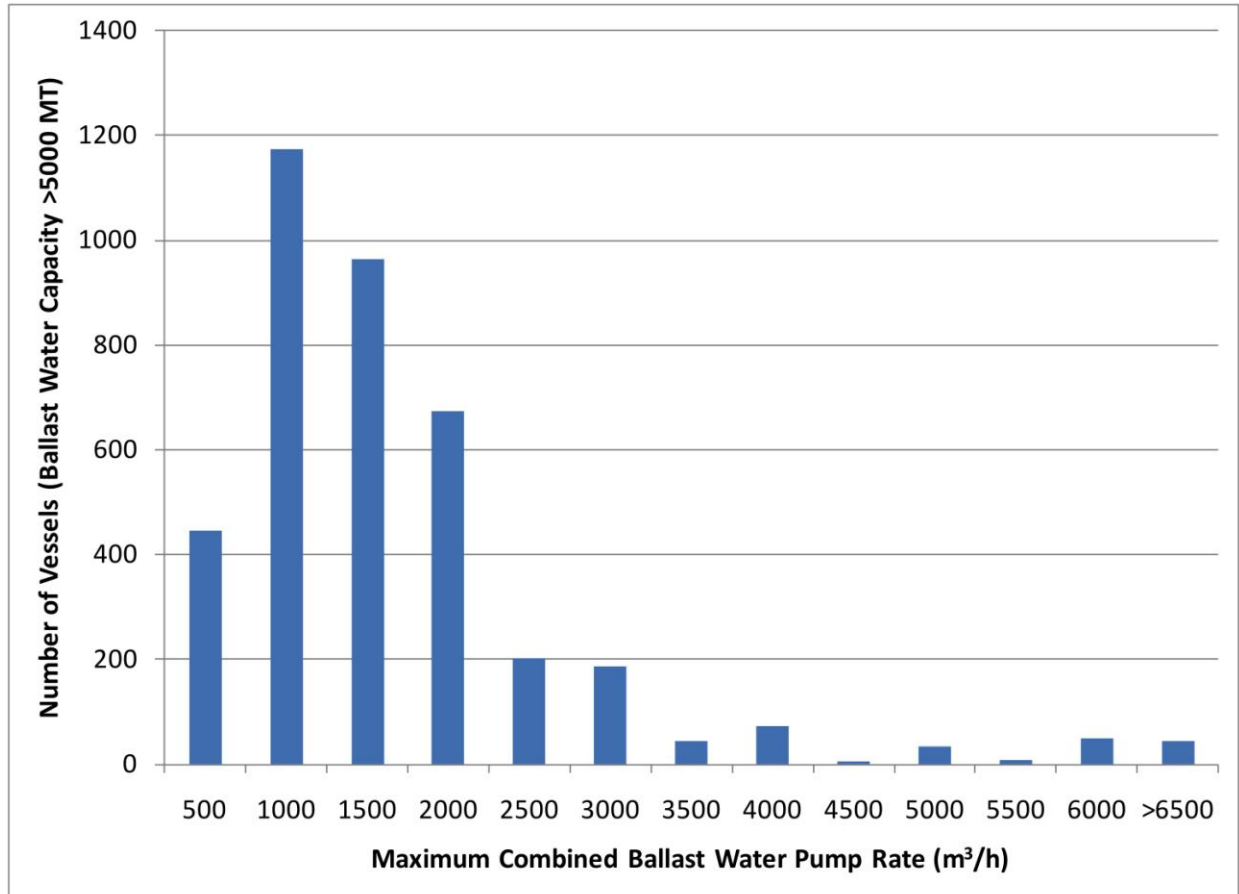
Shipboard estimate, treatment capacity: Figure A4-2 shows California State Lands Commission data on the ballast pump capacities in a sample of nearly 4,000 distinct ships arriving in California ports. The average ballast pump capacity estimated from this figure is 1,436 MT/h. With 13,115 distinct ships, this yields an estimate of nearly 19 million MT/h of treatment capacity that would need to be installed.

Figure A4-2. Total ballast pump capacities of ships that call at California ports. Source: California SLC 2010, Fig. VI-3.

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4



As mentioned, not all vessels discharge ballast water on arriving at a California port, so not all of the distinct arriving ships may need to install treatment plants. Thus these numbers might overestimate, perhaps substantially, the number of plants and the treatment capacity needed for shipboard treatment. How significant could this overestimation be? On average, only 20% of ship arrivals at California ports report discharging ballast water (California SLC 2010); however, there is no independent verification of whether ships have or have not discharged ballast water, and there are reasons to suspect that ships often fail to report some of their discharges. Glosten (2002) reported that they “were often told by agents and operators that their vessels never discharge ballast in Puget Sound. However, we found that almost every vessel surveyed discharged ballast at some point while they were in port, usually for trim and list control, while loading and off-loading cargo.” Glosten (2002) concluded that the under-reporting occurred because many ship operators mistakenly excluded such common practices from their definition of ballast discharge. However, there is also a financial incentive for ship operators to not report ballast discharges: a ship reporting that it intends to discharge ballast is more likely to have its ballast tanks sampled, which is an inconvenience that involves some risk of delay, and which at

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

1 least theoretically increases the chance that it will be found to be out of compliance and
2 subjected to penalties. Studies in Australia (Lockwood 1999), the Great Lakes (Reeves 1998)
3 and Washington (Harkless 2003; Lyles 2004) found evidence that ships routinely misreported
4 their ballast management activities (see also Cohen & Foster 2000 at footnote 163). Harkless
5 (2003) reported that some Chief Mates admitted that they intentionally reported false ballast
6 water information in order to satisfy regulators.

7
8 Even if the figure of ballast discharge by only 20% of California ship arrivals is accurate, much
9 more than 20% of the individual ships would probably need to install treatment plants to treat the
10 ballast discharged on *some* voyages. For example, if each ship discharged ballast on half of its
11 arrivals at California ports, then 100% of ships would need to treat ballast water even though
12 only 50% of arrivals involved ballast discharges. As a sensitivity test, we recalculated the
13 treatment plant and capacity estimates for California assuming the most extreme hypothetical
14 case of only 20% of arriving ships ever discharging ballast water in the state (Table A4-4;
15 compare to Table VI.B-2). In this case the number of treatment plants needed for shipboard
16 treatment is 164 times the number needed for onshore treatment (down from 820 in Table VI.B-
17 2) and the treatment capacity needed is 2,076 times the need with onshore treatment (down from
18 10,382 in Table VI.B-2). Though less, the difference is still striking.

19
20
21 **Table A4-4. Treatment plant and capacity estimates for the California, assuming that only 20% of ships**
22 **arriving in California ever discharge ballast water there.**
23

Site	Number of Treatment Plants		Total Capacity of Treatment Plants (MT/h)	
	Onshore	Shipboard	Onshore	Shipboard
California	16	2,623	1,814	3,766,628

24
25
26 United States
27

28 *Onshore estimate:* To estimate the number of onshore treatment plants and the treatment capacity
29 needed in the United States, we started with the estimates for California derived above. We then
30 multiplied these by the ratio between the estimated total ballast water discharge in the United
31 States (239,989,668 MT/y derived from Miller et al. 2007 by the methods described earlier, see
32 Table A4-5) and the estimated discharge in California (12,251,089 MT/y). This yielded an
33 estimate of 314 onshore treatment plants needed with a total treatment capacity of 35,549 MT/h.
34

35
36 **Table A4-5. Estimate of the total annual ballast water discharge into U.S. waters, compared to the estimate**
37 **for California.**
38

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Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

	Domestic			Foreign			Total
	Reported Discharge	Reporting Rate	Estimated Discharge	Reported Discharge	Reporting Rate	Estimated Discharge	Estimated Discharge
US 2004-05	183,792,889	48.9	375,854,579	73,720,328	70.8	104,124,757	479,979,336
US annual	–	–	187,927,290	–	–	52,062,379	239,989,668
CA annual	–	–	7,244,845	–	–	5,006,244	12,251,089

Shipboard estimate: Approximately 40,000 cargo ships (excluding barges) are estimated to be subject to ballast water discharge requirements in the United States over the three-year VGP period (Albert & Everett 2010; (Ryan Albert, pers. comm., SAB public conference call 10/26/2010). Adjusting the ship numbers for a 30-year period by adding only the expected number of replacement ships (a conservative adjustment) and assuming an average 25-year lifetime for a ship yields 83,200 distinct ships requiring 83,200 treatment plants. No data on ballast pump capacities comparable to the California data in Figure 2 are available for the U.S. as whole. We used California's average ballast pump capacity of 1,436 MT/h, to yield an estimate of total treatment capacity of 119 million MT/h need for shipboard treatment.

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Committee Augmented for Ballast Water

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Appendix 5. Cost Analysis

This appendix shows the source data and explains the calculations of the cost comparison in §VI.E “Cost of Onshore vs. Shipboard Treatment”. The assumptions and some common data used in these calculations are in Table A5-1. The inflation figures are based on the U.S. Bureau of Labor Statistics' Consumer Price Index for all Urban Consumers (CPI-U), as described in Appendix 2.

Table A5-1. Assumptions and some common data for the cost analysis.

0.05	Annual interest rate
30	Lifetime of onshore components (years)
25	Lifetime of new ship outfitted at the time of construction with treatment plants or with pipes and pumps to discharge ballast water onshore; shipboard plant, pipes and pumps assumed to have the same lifetime as the ship (years)
12.5	Remaining lifetime of old ships retrofitted with treatment plants or with pipes and pumps to discharge ballast water onshore; shipboard plant, pipes and pumps assumed to have the same lifetime as the ship (years)
1.2548	Inflation from 9/1/2000 to 6/1/2010 (from publication of CAPA 2000 to present)
1.2307	Inflation from 1/1/2002 to 6/1/2010 (from publication of Glosten 2002 to present)
0.9949	Inflation from 8/1/2008 to 6/1/2010 (from publication of Brown and Caldwell 2008 to present)
1.0056	Inflation from 2/1/2010 to 6/1/2010 (from publication of Lloyd's Register 2010 to present)
3,302,988	Total California ballast water discharge, as reported in CAPA 2000 (MT/y)
12,251,089	Total California ballast water discharge based on the most recent NBIC report, Miller et al. 2007 (covering 2004-05), foreign & domestic combined, adjusted for reporting rates (MT/y)
239,989,668	Total U.S. ballast water discharge based on the most recent NBIC report, Miller et al. 2007 (covering 2004-05), foreign & domestic combined, adjusted for reporting rates (MT/y)
3.7	Ratio of the California ballast water discharge estimate based on Miller et al. 2007 to the estimate in CAPA 2000
19.6	Ratio of the U.S. to the California ballast water discharge estimates based on Miller et al. 2007

California - Onshore Cost - (1) On-land Component

The original cost data from CAPA (2000) is shown in Table A5-2. Under Annualized Costs, the first column shows the figures from CAPA (2000) and the second column shows annualized costs calculated by the method described in Appendix 2.

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Committee Augmented for Ballast Water

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Table A5-2. Costs for onshore treatment in California from CAPA (2000), Tables 5.1 and 5.2.

Port	Capital Costs				Annual O&M	Annualized Costs	
	Pipes	Storage Tanks	Treatment Plants	Outfalls		CAPA	Calculated
Hueneme	1,056,000	55,000	0	100,000	0	40,367	78,777
Humboldt Bay	12,672,000	4,000,000	1,781,000	100,000	149,800	768,233	1,356,699
Long Beach	28,617,600	5,100,000	2,220,400	100,000	223,454	1,424,721	2,567,778
Los Angeles	27,033,600	20,400,000	2,220,400	100,000	223,454	1,881,921	3,460,023
Oakland	15,840,000	3,800,000	1,781,000	100,000	149,800	867,167	1,549,772
Redwood City	1,584,000	4,300,000	1,631,500	100,000	142,400	396,250	637,799
Richmond	5,808,000	3,400,000	1,631,500	100,000	142,400	507,050	854,030
Sacramento	1,372,800	4,800,000	1,631,500	100,000	142,400	405,877	656,586
San Diego	9,292,800	3,100,000	1,631,500	100,000	142,400	613,210	1,061,206
San Francisco	8,448,000	6,300,000	1,781,000	100,000	149,800	704,100	1,231,540
Stockton	5,385,600	5,500,000	1,631,500	100,000	142,400	562,970	963,160
Calif. Total	117,110,400	60,755,000	17,941,300	1,100,000	1,608,308	8,171,865	14,417,371

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Table A5-3 shows the costs from Table A5-2, not including the CAPA (2000) figures for annualized costs, adjusted for inflation.

Table A5-3. Costs for onshore treatment in California from CAPA (2000), adjusted for inflation.

Port	Capital Costs				Annual O&M	Annualized Costs
	Pipes	Storage Tanks	Treatment Plants	Outfalls		
Hueneme	1,325,069	69,014	0	125,480	0	98,850
Humboldt Bay	15,900,826	5,019,200	2,234,799	125,480	187,969	1,702,386
Long Beach	35,909,364	6,399,480	2,786,158	125,480	280,390	3,222,047
Los Angeles	33,921,761	25,597,920	2,786,158	125,480	280,390	4,341,637
Oakland	19,876,032	4,768,240	2,234,799	125,480	187,969	1,944,654
Redwood City	1,987,603	5,395,640	2,047,206	125,480	178,684	800,310
Richmond	7,287,878	4,266,320	2,047,206	125,480	178,684	1,071,637
Sacramento	1,722,589	6,023,040	2,047,206	125,480	178,684	823,884
San Diego	11,660,605	3,889,880	2,047,206	125,480	178,684	1,331,601
San Francisco	10,600,550	7,905,240	2,234,799	125,480	187,969	1,545,337
Stockton	6,757,851	6,901,400	2,047,206	125,480	178,684	1,208,574
Calif. Total	146,950,130	76,235,374	22,512,743	1,380,280	2,018,105	18,090,918

Table A5-4 shows the costs from Table A5-3, with various adjustments to correspond to a 3.7x higher estimate of ballast water discharge than was used in CAPA (2000). These include the following:

- *Pipe Capital Costs*: Costs from Table A5-3 were adjusted by (1) multiplying the maximum discharge/day for each port (from CAPA 2000, Table 4.4) by 3.7; (2) selecting the least-cost set of pipe sizes from Brown and Caldwell (2007, Table 4) that are capable of handling the adjusted maximum discharge/day, expressed as gallons per minute (gpm); (3) multiplying the construction cost per lineal foot (Brown and Caldwell 2007, Table 4) times the total length of pipe needed at that port (CAPA 2000, Table 4.2); adding 25% for contingency and 30% for technical services; and inflating to June 1, 2010 dollars. The details of the pipe calculations are shown below in Table A5-5.

- *Storage Tank and Outfall Capital Costs, and Annual O&M*: Costs from Table A5-3 were multiplied by 3.7. This may be an overestimate (especially for capital costs) because it fails to account for economies of scale.

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Committee Augmented for Ballast Water

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1
2 • *Treatment Plant Capital Costs*: Costs from Table A5-3 were adjusted by multiplying the
3 required treatment capacity for each port (CAPA 2000: Table 4.5) by the ratio between our best
4 estimate of California BW discharge and CAPA's estimate, selecting the least-cost set of
5 treatment plant sizes from CAPA 2000: Table 4.7 that can handle the adjusted required treatment
6 capacity, and inflating to June 1, 2010 dollars. Includes 30% contingency. This is probably an
7 overestimate because it fails to account for economies of scale in the larger plants. The details of
8 the pipe calculations are shown below in Table A5-6.
9

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Committee Augmented for Ballast Water

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Table A5-4. Costs for onshore treatment in California from CAPA (2000), adjusted for inflation and to an updated estimate for California ballast water discharge.

Port	Capital Costs				Annual O&M	Annualized Costs
	Pipes	Storage Tanks	Treatment Plants	Outfalls		
Hueneme	1,245,877	255,979	0	465,417	0	127,974
Humboldt Bay	34,350,611	18,616,679	2,786,158	465,417	697,195	4,354,312
Long Beach	77,600,343	23,736,265	8,358,474	465,417	1,039,993	8,206,091
Los Angeles	238,318,485	94,945,061	11,144,632	465,417	1,039,993	23,474,515
Oakland	42,893,768	17,685,845	2,786,158	465,417	697,195	4,849,505
Redwood City	3,737,631	20,012,929	2,786,158	465,417	662,754	2,419,281
Richmond	15,840,437	15,824,177	2,234,799	465,417	662,754	2,898,235
Sacramento	3,737,631	22,340,014	2,786,158	465,417	662,754	2,570,662
San Diego	20,534,724	14,427,926	2,786,158	465,417	662,754	3,148,644
San Francisco	22,959,735	29,321,269	2,786,158	465,417	697,195	4,309,669
Stockton	14,594,560	25,597,933	2,234,799	465,417	662,754	3,452,986
Calif. Total	475,813,801	282,764,077	40,689,651	5,119,587	7,485,338	59,811,874

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Table A5-5. Estimate of Pipe Capital Costs for onshore treatment in California. CAPA Maximum Discharge is from CAPA (2000), Table 4.4. Adjusted Maximum Discharge is CAPA Maximum Discharge multiplied by 3.7 and expressed as gpm. Pipe Capacity and Pipe Diameter are the pipe sizes from Brown and Caldwell (2007), Table 4 needed to handle the Adjusted Maximum Discharge (3 of the available sizes of pipes are need for the Port of Los Angeles), and Unit Construction Cost is from the same table. Pipe Length is from CAPA (2000), Table 5.1. Total Capital Cost is Unit Construction Cost times Pipe Length, adjusted for inflation.

Port	CAPA Maximum Discharge (gpd)	Adjusted Maximum Discharge (gpm)	Pipe Capacity (gpm)	Pipe Diameter (in)	Unit Construction Cost (lineal foot)	Pipe Length (km)	Total Capital Cost
Hueneme	54,128	139	1,000	10	140	1.6	1,245,877
Humboldt Bay	3,944,058	10,159	16,667	36	320	19.3	34,350,611
Long Beach	5,104,821	13,149	16,667	36	320	43.6	77,600,343
Los Angeles #1			25,000	42	440		
Los Angeles #2	20,285,271	52,250	25,000	42	440	41.2	238,318,485
Los Angeles #3			3,000	16	160		
Oakland	3,667,472	9,447	16,667	36	320	24	42,893,768
Redwood City	4,181,547	10,771	16,667	36	320	2	3,737,631
Richmond	3,312,692	8,533	16,667	36	320	9	15,840,437
Sacramento	4,711,895	12,137	16,667	36	320	2	3,737,631
San Diego	3,016,584	7,770	8,333	30	260	14	20,534,724
San Francisco	6,202,051	15,975	16,667	36	320	13	22,959,735
Stockton	5,469,666	14,089	16,667	36	320	8	14,594,560
Calif. Total	59,950,185	154,417	195,669	—	—	178	475,813,801

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Committee Augmented for Ballast Water

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Table A5-6. Estimate of Treatment Plant Capital Costs for onshore treatment in California. CAPA Required Treatment Capacity is from CAPA (2000), Table 4.5. Adjusted Required Treatment Capacity is CAPA Required Treatment Capacity multiplied by 3.7. Treatment Plant Size is the minimum plant size as a multiple of the plant sizes whose costs were estimated in CAPA (2000) (0.1, 0.2 and 1.0 mgd), and Plant Cost is the cost estimated as multiples of the CAPA (2000) plant costs (i.e. the cost of a 3 mgd plant is estimated as 3 times CAPA's cost estimate for a 1 mgd plant), adjusted for inflation.

Port	CAPA Required Treatment Capacity (gpd)	Adjusted Required Treatment Capacity (gpd)	Treatment Plant Size (mgd)	Plant Cost
Hueneme	497	1,843	—	—
Humboldt Bay	140,084	519,585	1	2,786,158
Long Beach	679,714	2,521,122	3	8,358,474
Los Angeles	993,539	3,685,128	4	11,144,632
Oakland	159,694	592,320	1	2,786,158
Redwood City	56,493	209,538	1	2,786,158
Richmond	44,269	164,198	0.2	2,234,799
Sacramento	99,306	368,335	1	2,786,158
San Diego	56,986	211,366	1	2,786,158
San Francisco	109,124	404,751	1	2,786,158
Stockton	50,843	188,581	0.2	2,234,799
California Total	2,390,549	8,866,768	13.4	40,689,651

The area needed for storage tanks was estimated as shown in Table A5-7, and the area needed for treatment plants was estimated as 0.25 acres for a 0.2 mgd plant, and 1 acre/mgd for plants ≥ 1 mgd. Land Costs were estimated as shown in Table A5-8, with supporting data shown in Table A5-9. Land costs were added to the Storage and Treatment Plant capital costs in Table A5-4 to produce Table A5-10.

12/10/2010 Science Advisory Board (SAB) Ecological Processes and Effects
Committee Augmented for Ballast Water

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Subgroup 4. Onshore Treatment, inclusion in response to Question 4

Table A5-7. Estimate of land needed for storage tanks for onshore treatment in California. CAPA Storage Needed is from CAPA (2000), Table 4.5. Adjusted Storage Needed is CAPA Storage Needed multiplied by 3.7. Number of Tanks is the minimum number of steel tanks of 7.3 m height and 60 m maximum diameter needed to provide the Adjusted Storage Needed. Tank Diameter gives the corresponding tank diameters. Tank Area is the area needed if each tank occupies a square with a 1 m buffer (i.e. a square whose sides equal the tank diameter plus 2 m).

Port	CAPA Storage Needed (gal)	Adjusted Storage Needed (gal)	Number of Tanks	Tank Diameter (m)	Tank Area (acres)
Hueneme	108,257	401,535	1	16.3	0.08
Humboldt Bay	7,888,116	29,257,755	6	56.7	5.1
Long Beach	10,209,642	37,868,510	7	59.8	6.6
Los Angeles	40,570,700	150,480,492	28	59.6	26.2
Oakland	7,334,944	27,205,989	5	59.9	4.7
Redwood City	8,363,094	31,019,491	6	58.4	5.4
Richmond	6,625,384	24,574,163	5	57.0	4.3
Sacramento	9,423,472	34,952,533	7	57.4	6.1
San Diego	6,033,114	22,377,381	5	54.4	3.9
San Francisco	12,403,838	46,006,987	9	58.1	8.0
Stockton	10,939,280	40,574,804	8	57.9	7.1
California Total	119,899,842	444,719,639	87	—	77.6

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Committee Augmented for Ballast Water

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Table A5-8. Estimate of land costs for onshore treatment in California. Per acre land costs were estimated from the records in Table A5-9.

Port	Storage Tank Area (acres)	Treatment Plant Area (acres)	Land Cost per acre	Land Cost - Storage	Land Cost-Treatment
Hueneme	0.08	–	500,000	41,295	0
Humboldt Bay	5.1	1	700,000	3,580,950	700,000
Long Beach	6.6	3	1,000,000	6,598,423	3,000,000
Los Angeles	26.2	4	2,000,000	52,452,334	8,000,000
Oakland	4.7	1	700,000	3,317,746	700,000
Redwood City	5.4	1	500,000	2,706,521	500,000
Richmond	4.3	.25	500,000	2,147,790	125,000
Sacramento	6.1	1	500,000	3,053,230	500,000
San Diego	3.9	1	1,000,000	3,924,311	1,000,000
San Francisco	8.0	1	2,000,000	16,062,874	2,000,000
Stockton	7.1	.25	100,000	708,500	25,000
California Total	77.6	13.5	–	94,593,975	16,550,000

Table A5-9. Price of vacant industrial or commercial land offered for sale near ports. From <http://www.cityfeet.com>, accessed 12/1/10.

Port	Acres in parcel	Price per acre	Port	Acres in parcel	Price per acre
Humboldt Bay	3	633,333	Oakland	1	795,000
Humboldt Bay	2	604,167	Oakland	2.9	1,818,182
Long Beach	5.6	1,094,643	Redwood City	1	1,475,000
Long Beach	12.4	958,237	Redwood City	0.4	547,945
Los Angeles	1.0	932,697	Richmond	1	398,000
Los Angeles	1.0	1,350,000	Sacramento	4	381,150
Los Angeles	2.0	3,750,000	San Francisco	1.5	1,503,881
Oakland	19	684,211	Stockton	3	77,746

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Committee Augmented for Ballast Water

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Table A5-10. Costs for onshore treatment in California from CAPA (2000), adjusted for inflation and to an updated estimate for California ballast water discharge, including land costs.

Port	Capital Costs				Annual O&M	Annualized Costs
	Pipes	Storage Tanks	Treatment Plants	Outfalls		
Hueneme	1,245,877	297,274	0	465,417	0	130,660
Humboldt Bay	34,350,611	22,197,629	3,486,158	465,417	697,195	4,632,794
Long Beach	77,600,343	30,334,688	11,358,474	465,417	1,039,993	8,830,483
Los Angeles	238,318,485	147,397,394	19,144,632	465,417	1,039,993	27,407,026
Oakland	42,893,768	21,003,591	3,486,158	465,417	697,195	5,110,865
Redwood City	3,737,631	22,719,451	3,286,158	465,417	662,754	2,627,870
Richmond	15,840,437	17,971,967	2,359,799	465,417	662,754	3,046,083
Sacramento	3,737,631	25,393,244	3,286,158	465,417	662,754	2,801,804
San Diego	20,534,724	18,352,237	3,786,158	465,417	662,754	3,468,977
San Francisco	22,959,735	45,384,143	4,786,158	465,417	697,195	5,484,684
Stockton	14,594,560	26,306,433	2,259,799	465,417	662,754	3,500,701
Calif. Total	475,813,801	377,358,051	57,239,651	5,119,587	7,485,338	67,041,950

California - Onshore Cost - (2) Ship Retrofit/Modification

[To be completed]

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